

PURCHASING / PRODUCTION

HIGH PERFORMANCE CLOSED DIE FORGINGS

PURCHASE ORDER

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098252

the

What

recycle?

for

available

wastewater

and/or

process source?

PH. 216/477-4511

DATE

FAX 216/477-2046

PAGE 5/15/97 $\mathcal{Q}_{p}^{p,q}$

8529

VENDOR

TO:

PARSONS ENGINEERING -PF

19101 VILLAVIEW RD

STE 301

CANTON DROP FORGE

4575 SOUTHWAY ST., S.W.

CLEVELAND

OH 44119

P.O. BOX 6902

CANTON, OHIO 44706

CANTON DROP FORGE

4575 SOUTHWAY STREET S.W

P.O. BOX 6902

CANTON OH: 44706

STOCK ROOM

UNLESS OTHERWISE NOTED, SALES TAX DOES NOT APPLY ON ITEMS ORDERED

SHIP VIA:

-- RFST- UAY

FREIGHT TERMS:

	NEST STATE					
	NO. ITEM NO.	DESCRIPTION/COMMENTS	U/M	PROMISED OU DATE OR	ANTITY UNIT COST	TOTAL COST
	1 2 3 4	ENGINEERING ASSISTANCE FOR RECYCLING/TREA OF STEAM CONDENSATE WHICH IS AN OILY EMUL SCOPE OF WORK TO BE AS PROPOSED ON MAY 7, PROPOSAL VIA LETTER FROM MICHAEL R. LEFFL	SION. 1997			
	0 0 F 8 F 5	COST NOT TO EXCEED \$7,000.00 CONFIRMED BY KEITH HOUSEKNECHT 5/8/97				CDF002326
	6/26/97-7	8.04 ESCROW RED. KH1062 Purchase 25/47-6/6/97-7/07	Order Total			.00
	8/1/97-	Purchase 155147-6/16/97-2497,5 155157-7/8/97-3692.8	5 / Mrai	6/27	7) saed	
					Control of the contro	
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ALL ORDERS:

Terms and Conditions on reverse side are part of this Purchase Order.

Acceptance — Unless otherwise stated herein, this order must be accepted by the Selfer signing and returning the attached acknowledgment copy to Buyer within 10 days from the date of this order, and it is understood that

STEEL ORDERS:

Certifled test reports in triplicate are to accompany steel shipments. Discount will be taken from date of receipt of goods or test reports, whichever is later.

2. Do not deviate from established producing practice in fulfulf-

INVOICE DAY OF SHIPMENT TO: CANTON DROP FORGE PO. BOX 6902

OH 44706

ö What sources of volumes of each volumes required N

REMIT PAYMENT TO: File 91849 Los Angeles, CA 90074-1849 Attn: Accounts Receivables

Street Address: 19101 VILLAVIEW ROAD, SUITE 301 CLEVELAND, OHIO 44119

Tel: (216) 486-9005 Fax: (216) 486-6119

INVOICE

a(b),3

JULY 8, 1997

CLIENT REF. :

INVOICE NO. :

00755151

PROJECT NO. :

731549-T1

CLIENT NO. :

71275

TO: CANTON DROP FORGE, INC.

4575 SOUTHWAY STREET

CANTON, OHIO

44706

PLEASE REMIT TO:

PARSONS ENGINEERING SCIENCE, INC

FILE 91849

LOS ANGELES, CALIFORNIA

90074-1849

FOR: CANTON DROP FORGE, WASTEWATER RECYCLING

AUTHORIZATION: P.O. #98252 WBS 01000 - INVESTIGATION AMOUNT AUTHORIZED: \$7,000.00

ATTN: MR. KEITH HOUSEKNECHT

BILLING PERIOD: 5/31/97 THROUGH 6/27/97

	CUR. HOURS	CURRENT PERIOD THROUGH 6/27/97	CUM. HOURS	THROUGH 6/27/97
		<u> </u>		·
WBS 01000 - INVESTIGATION				
DIRECT LABOR	29.1	\$1,075.27	52.6	\$1,896.26
OH & PROFIT @1.95 X D.L.		\$2,096.78		\$3,697.71
ODCS WITHOUT HANDLING		\$.00		\$75.63
ODCS W/HANDLING Rate		\$496.00		\$496.00
Markup: 5%		\$24.80		\$24.80
SUBTOTA	Т:	\$3,692.85		\$6,190.40
TOTAL THIS INVOICE	E:	\$\$3,692.85	Q در	\$6,190.40
		Ani 7/2	29/97	
		0 "		

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2(b)

CLIENT REF .:

INVOICE NO.: 00755151
PROJECT NO.: 731549-T1
CLIENT NO.: 71275

FORMAT NAME: SBLRLBR15C

	EMPLOYEE NAME	ADJ. DATE	REGULAR HOURS	O/T HOURS	TOTAL HOURS	BILLING RATE	LABOR BILLING	PREMIUM BILLING
25	SENIOR SPECIALIST II							
	STEPHEN E HALL	05/23/97	.50		.50	35.68	17.05	
	CLASSIFICATION TOTALS		.50		.50		17.85	
35	SPVG SPECIALIST II							
	MICHELLE MCDONALD		.10		.10	56.64	5.66	
	CLASSIFICATION TOTALS	-	.10		.10		5.66	
			-					
90	PRINC ENG/SCIENTIST 1							
	MICHAEL R LEFFLER		27.00		27.00	109.80	2,964.75	
	DAVID G JOHNSON		1,50		1.50	122.52	183.79	
•	CLASSIFICATION TOTALS		28.50		28.50		3,148.54	
	TOTAL LABOR BILLING		29.10		29.10		3,172.05	

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INVOICE NO.: 00755151
PROJECT NO.: 731549-T1

CLIENT NO..: 71275

CLIENT REF .:

FORMAT NAME: SBLRLBR11C

			ADJ.		REGULAR	T\O	TOTAL.
W/E DATE	EMPLOYEE NAME	EMPLOYEE CLASSIFICATION	DATE	RATE	HOURS	HOURS	HOURS
010	00 INVESTIGATION				•		
6/06/97	MICHAEL R LEFFLER	PRINC ENG/SCIENTIST I		109.80	14.00		14.00
6/13/97	MICHELLE MCDONALD	SFVG SPECIALIST II		56.64	.10		.10
6/13/97	MICHAEL R LEFFLER	PRINC ENG/SCIENTIST I		109.80	9.00	:	9.00
6/13/97	DAVID G JOHNSON	PRINC ENG/SCIENTIST I		122.52	1.50		1.50
6/20/97	STEPHEN E HALL	SENIOR SPECIALIST II	05/23/97	35.68	.50		.50
6/20/97	MICHAEL R LEFFLER	PRINC ENG/SCIENTIST I		109.80	4.00		4.00
	ITEM TOTALS				29.10		29.10
	TOTAL LABOR HOURS				29,10		29.10

2(6),

PAGE:

DETAIL OF OTHER DIRECT COSTS
FOR THE PERIOD ENDING 6/27/97
BY WBS/COST CODE

INVOICE NO.: 00755151
PROJECT NO.: 731549-T1
CLIENT NO.: 71275

CLIENT NO... /12/3

FORMAT NAME: SBLRFODC03

REF:

REFERENCE NUMBER	AMOUNT		
01000: INVESTIGATION		-	
9600	TEMP SERVICES & CONSULT	.00	
9.605	CONSULTING SERVICES-LIFE SCIENCE LABORAT	150.00	
9605	CONSULTING SERVICES-QUANTERRA, INC.	346.00	
	INVESTIGATION	496.00	
	GRAND TOTAL OTHER DIRECT COSTS	496.00	

PAGE:

496.00

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 6/27/97 BY JOB/WBS/COST CODE

CLIENT REF.:

INNOICE NO.: 00755151
PROJECT NO.: 731549-T1
CLIENT NO.: 71275
FORMAT NAME: SBLRODCWTT

2(6)

EQUIP/ REF VEND INVOICE DATE BATCH ио. NO. NAME DATE WORKED DESCRIPTION NO. AMOUNT 731549 CANTON DROP FORGE, WASTEWATER 01000 INVESTIGATION 9605 CONSULTING SERVICES 512 150.00 069705690 J4277 LIFE SCIENCE LABORATORIES 5/23/97 391 346.00 069706578 J6306 QUANTERRA, INC. 6/04/97 496.00 ACCOUNT TOTAL 496.00 INVESTIGATION JOB 731549 TOTAL 496.00

TOTAL, OTHER DIRECT COSTS

REMIT PAYMENT TO: File 91849 Los Angeles, CA 90074-1849 Attn: Accounts Receivables

Street Address: 19101 VILLAVIEW ROAD, SUITE 301 CLEVELAND, OHIO 44119

Tel: (216) 486-9005 Fax: (216) 486-6119

INVOICE

JULY 8, 1997

CLIENT REF. :

INVOICE NO. : PROJECT NO. :

00755151 731549-T1

CLIENT NO. :

71275

TO: CANTON DROP FORGE, INC.

4575 SOUTHWAY STREET

CANTON, OHIO

44706

PLEASE REMIT TO:

PARSONS ENGINEERING SCIENCE, INC

FILE 91849

LOS ANGELES, CALIFORNIA

90074-1849

FOR: CANTON DROP FORGE, WASTEWATER RECYCLING

AUTHORIZATION: P.O. #98252 WBS 01000 - INVESTIGATION AMOUNT AUTHORIZED: \$7,000.00

ATTN: MR. KEITH HOUSEKNECHT

BILLING PERIOD: 5/31/97 THROUGH 6/27/97

	CUR. Hours	CURRENT PERIOD THROUGH 6/27/97	CUM. HOURS	CUMULATIVE-TO-DATE THROUGH 6/27/97
	·			·
WBS 01000 - INVESTIGATION				
DIRECT LABOR	29.1	\$1,075.27	52.6	\$1,896.26
OH & PROFIT @1.95 X D.L.		\$2,096.78		\$3,697.71
ODCS WITHOUT HANDLING		\$.00		\$75.63
ODCS W/HANDLING Rate		\$496.00		\$496.00
Markup: 5%		\$24.80		\$24.80
SUBTOTAL	·:	\$3,692.85		\$6,190.40
TOTAL THIS INVOICE	E:	\$3,692.85		\$6,190.40

DETAIL OF PROFESSIONAL SERVICES FOR THE PERIOD ENDING 6/27/97

CLIENT REF.:

INVOICE NO.: 00755151 PROJECT NO.: 731549-T1 CLIENT NO..: 71275 FORMAT NAME: SBLRLBR15C

	EMPLOYEE NAME	ADJ. DATE	REGULAR HOURS	O/T HOURS	TOTAL HOURS	BILLING RATE	LABOR BILLING	PREMIUM BILLING
25	SENIOR SPECIALIST II							
	STEPHEN E HALL	05/23/97	.50		.50	35.68	17.85	
	CLASSIFICATION TOTALS	3	. 50		.50		17.85	ı
35	SPVG SPECIALIST II							
	MICHELLE MCDONALD		.10		.10	56.64	5.66	
	CLASSIFICATION TOTAL	S	.10		.10		5.66	-
90	PRINC ENG/SCIENTIST I							
	MICHAEL R LEFFLER		27.00		27.00	109.80	2,964.75	
	DAVID G JOHNSON		1.50		1.50	122.52	183.79	
	CLASSIFICATION TOTAL	28	28.50		28.50		3,148.54	
	TOTAL LABOR BILLING		29.10		29.10	•	3,172.05	

DETAIL OF PROFESSIONAL SERVICES FOR THE PERIOD ENDING 6/27/97

CLIENT REF .:

INVOICE NO.: 00755151
PROJECT NO.: 731549-T1
CLIENT NO..: 71275
FORMAT NAME: SBLRLBR11C

W/E DATE	EMPLOYEE NAME	EMPLOYEE CLASSIFICATION	ADJ. DATE	RATE	REGULAR HOURS	O/T HOURS	TOTAL HOURS
WE DATE	EMPLOTEE MAND	ENTROTES CLASSIFICATION				110010	
010	00 INVESTIGATION						
6/06/97	MICHAEL R LEFFLER	PRINC ENG/SCIENTIST I		109.80	14.00		14.00
6/13/97	MICHELLE MCDONALD	SPVG SPECIALIST II		56.64	.10		.10
6/13/97	MICHAEL R LEFFLER	PRINC ENG/SCIENTIST I		109.80	9.00		9.00
6/13/97	DAVID G JOHNSON	PRINC ENG/SCIENTIST I		122.52	1.50		1.50
6/20/97	STEPHEN E HALL	SENIOR SPECIALIST II	05/23/97	35.68	.50		.50
6/20/97	MICHAEL R LEFFLER	PRINC ENG/SCIENTIST I		109.80	4.00		4.00
	ITEM TOTALS				29.10		29.10
	TOTAL LABOR HOURS		-		29.10		29.10

PAGE: 1

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 6/27/97 BY WBS/COST CODE INVOICE NO.: 00755151 PROJECT NO.: 731549-T1 CLIENT NO.: 71275

FORMAT NAME: SBLRFODC03

REF:

REFERENCE NUMBER	DESCRIPTION OF EXPENSES	AMOUNT	
01000: INVESTIGATION			
9600	TEMP SERVICES & CONSULT	.00	
9605	CONSULTING SERVICES-LIFE SCIENCE LABORAT	150.00	
9605	CONSULTING SERVICES-QUANTERRA, INC.	346.00	
	INVESTIGATION	496.00	
	GRAND TOTAL OTHER DIRECT COSTS	496.00	

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 6/27/97 BY JOB/WBS/COST CODE

CLIENT REF .:

INVOICE NO.: 00755151
PROJECT NO.: 731549-T1
CLIENT NO.: 71275

FORMAT NAME: SBLRODCWTT

	EQUIP/						
REF	VEND		INVOICE	DATE		BATCH	_
ио.	NO.	NAME	DATE	WORKED	DESCRIPTION	ио.	THUOMA
731549	CANTON DROP FORGE	WASTEWATER					
0100	0 INVESTIGATION						
	9605 CONSULTING S	ERVICES					
06970569	90 J4277 LIFE SCIENC	E LABORATORIES	5/23/97			512	150.00
0697065	78 J6306 QUANTERRA,	INC.	6/04/97			391	346.00
					ACCOUNT TOTAL		496.00
	·				INVESTIGATION		496.00
÷					JOB 731549 TOTAL		496.00
				TOTAL,	OTHER DIRECT COSTS		496.00



REMIT PAYMENT TO: File 91849 Los Angeles, CA 90074-1849 Attn: Accounts Receivables

Street Address: 19101 VILLAVIEW ROAD, SUITE 301 CLEVELAND, OHIO 44119

Tel: (216) 486-9005 Fax: (216) 486-6119

INVOICE

26

AUGUST 8, 1997

CLIENT REF. :

INVOICE NO. :

00810971

PROJECT NO. :

731549-T1

CLIENT NO.

71275

TO: CANTON DROP FORGE, INC. 4575 SOUTHWAY STREET

CANTON, OHIO

44706

PLEASE REMIT TO:

PARSONS ENGINEERING SCIENCE, INC

FILE 91849

LOS ANGELES, CALIFORNIA

90074-1849

FOR: CANTON DROP FORGE, WASTEWATER RECYCLING

AUTHORIZATION: P.O. #98252 WBS 01000 - INVESTIGATION AMOUNT AUTHORIZED: \$7,000.00

ATTN: MR. KEITH HOUSEKNECHT

BILLING PERIOD: 6/28/97 THROUGH 7/25/97

	CUR. HOURS		ERIOD /25/97	CUM. HOURS	CUMULATIV THROUGH	E-TO-DATE 7/25/97
						<u> </u>
WBS 01000 - INVESTIGATION					•	
DIRECT LABOR			\$.00	52.6		\$1,896.26
OH & PROFIT @1.95 X D.L.	-		\$.00			\$3,697.71
ODCS WITHOUT HANDLING		\$	3127.60			\$203.23
ODCS W/HANDLING Rate			\$.00			\$496.00
Markup: 5%			\$.00			\$24.80
SUBTOTA	L:		\$127.60			\$6,318.00
TOTAL THIS INVOIC	E:		\$127.60			\$6,318.00
					=======	

PAGE:

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 7/25/97 BY WBS/COST CODE

PROJECT NO.: 731549-T1 CLIENT NO..: 71275

FORMAT NAME: SBLRFODC03

INVOICE NO.: 00810971

REFERENCE NUMBER	EFERENCE NUMBER DESCRIPTION OF EXPENSES		
01000: INVESTIGATION			
9540	FREIGHT/EXPRESS/POSTAGE	112.08	
9550	REPRODUCTION CHARGES	4.80	
9560	COMMUNICATIONS	10.72	
	INVESTIGATION	127.60	
	GRAND TOTAL OTHER DIRECT COSTS	127.60	

DETAIL OF OTHER DIRECT COSTS

FOR THE PERIOD ENDING 7/25/97

BY JOB/WBS/COST CODE

CLIENT REF.:

INVOICE NO.: 00810971
PROJECT NO.: 731549-T1
CLIENT NO.: 71275
FORMAT NAME: SBLRODCWTT

EQUIP/

	EQUIPY							
REF	VEND			INVOICE	DATE		BATCH	
NO.	NO.	NAME		DATE	WORKED	DESCRIPTION	NO.	AMOUNT
								
704540								
731549	CANTON DROP FO	ORGE, WASTEWAT	ER					
5100	o							
0100	0 INVESTIGATIO	ON						
	9542 EXPRESS							
•	9542 EXPRESS							
06970573	0 J2681 FEDERAL	PVDabge/II e	COLLEGETO	6/10/07				
	5 A4337 FEDERAL		COLLECTIO				512	8.67
	5 A4337 FEDERAL			5/23/97 5/23/97			387	51.41
	S TOO TESSION	BACKBOD		3/23/3/		ACCOUNT TOTAL	387	49.80
						ACCOONT TOTAL	•	109.88
	9543 POSTAGE							
	00052				6/26/97	POSTAGE	486	.32
	00052					POSTAGE	486	.78
	00052					POSTAGE	86	.78
	00052					POSTAGE	86	.32
						ACCOUNT TOTAL		2.20
	•							
	9551 COPIER C	CHARGES						
						•		
	30270				6/20/97	COPIER CHARGES	93	1.40
	30270				6/20/97	COPIER CHARGES	93	.40
	30270		,		6/20/97	COPIER CHARGES	93	.60
	30270				6/26/97	COPIER CHARGES	99	1.20
	30270				7/18/97	COPIER CHARGES	94	1.20
						ACCOUNT TOTAL		4.80
	9561 TELEPHON	NE CHARGES						
	6		•			(C)		
	00051				6/20/97	TELEPHONE CHARGES	102	1.82
	00051				6/20/97	TELEPHONE CHARGES	102	.44
	00031	•			7/11/97	TELEPHONE CHARGES	85	.43
	00051				7/18/97	7 TELEPHONE CHARGES	86	1.03
						ACCOUNT TOTAL		3.72
	9562 FAX CHA	RGES						
		•						
	00015					7 FAX CHARGES	81	3.00
	00015				6/13/9	7 FAX CHARGES	81	4.00

PAGE:

DETAIL OF OTHER DIRECT COSTS

PAGE:

FOR THE PERIOD ENDING 7/25/97 BY JOB/WBS/COST CODE

CLIENT REF .:

INVOICE NO.: 00810971
PROJECT NO.: 731549-T1
CLIENT NO.: 71275
FORMAT NAME: SBLRODCWTT

EQUIP/

REF	VEND		INVOICE	DATE			BATCH	
NO.	NO.	NAME	DATE	WORKED	DES	SCRIPTION	. ОИ	AMOUNT
			±		ACCOUNT TOTA	AL		7.00
					INVESTIGATIO	ON		127.60
					JOB 731549 1	TOTAL		127.60
				TOTAL,	OTHER DIRECT	COSTS		127.60



REMIT PAYMENT TO: File 91849 Los Angeles, CA 90074-1849 Altn: Accounts Receivables

Street Address: 19101 VILLAVIEW ROAD, SUITE 301 CLEVELAND, OHIO 44119

Tel: (216) 486-9005 Fax: (216) 486-6119

INVOICE

2(6), 3

OCTOBER 13, 1997

CLIENT REF. :

INVOICE NO. :

00870845

PROJECT NO. :

731549-T1

CLIENT NO. :

71275

TO: CANTON DROP FORGE, INC. 4575 SOUTHWAY STREET

CANTON, OHIO

44706

PLEASE REMIT TO:

PARSONS ENGINEERING SCIENCE, INC

FILE 91849

LOS ANGELES, CALIFORNIA

90074-1849

FOR: CANTON DROP FORGE, WASTEWATER RECYCLING

AUTHORIZATION: P.O. #98252 WBS 01000 - INVESTIGATION AMOUNT AUTHORIZED: \$7,000.00

ATTN: MR. KEITH HOUSEKNECHT

BILLING PERIOD: 8/30/97 THROUGH 9/26/97

	CUR. HOURS	CURRENT PERIOD THROUGH 9/26/97	CUM. HOURS	CUMULATIVE-TO-DATE THROUGH 9/26/97
WBS 01000 - INVESTIGATION DIRECT LABOR	2.0	\$74.44	56.6	***
OH & PROFIT @1.95 X D.L.	2.0	\$145.16	56.6	\$2,018.11 \$3,935.32
ODCS WITHOUT HANDLING		\$13.74		\$3,933.32 \$218.75
ODCS W/HANDLING Rate		\$.00		\$496.00
Markup: 5%	•	\$.00		\$24.80
SUBTOTAL	\$233.34		\$6,692.98	
TOTAL THIS INVOICE	:	\$233.34		\$6,692.98
				*======================================

CLIENT REF.:

INVOICE NO.: 00870845

PROJECT NO.: 731549-T1

CLIENT NO..: 71275

FORMAT NAME: SBLRLBR15C

		ADJ.	REGULAR	O/T	TOTAL	BILLING	LABOR	PREMIUM
	EMPLOYEE NAME	DATE	HOURS	HOURS	HOURS	RATE	BILLLING	BILLING
90	PRINC ENG/SCIENTIST I							
	MICHAEL R LEFFLER	09/05/97	2.00		2.00	109.80	219.60	
	CLASSIFICATION TOTALS		2.00		2.00		219.60	
	TOTAL LABOR BILLING		2.00		2.00		219.60	

PAGE: 3

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 9/26/97 BY WBS/COST CODE INVOICE NO.: 00870845
PROJECT NO.: 731549-T1
CLIENT NO.: 71275

FORMAT NAME: SBLRFODC03

REF:

REFERENCE NUMBER	DESCRIPTION OF EXPENSES	AMOUNT
01000: INVESTIGATION		-~
9540	FREIGHT/EXPRESS/POSTAGE	1.24
9550	REPRODUCTION CHARGES	2.50
9570	CAD/GIS/COMPUTERS	10.00
	INVESTIGATION	13.74
	GRAND TOTAL OTHER DIRECT COSTS	13.74

DETAIL OF OTHER DIRECT COSTS

PAGE:

1

FOR THE PERIOD ENDING 9/26/97 BY JOB/WBS/COST CODE

CLIENT REF.:

INVOICE NO.: 00870845
PROJECT NO.: 731549-T1
CLIENT NO..: 71275

FORMAT NAME: SBLRODOWTT

EQUIP/

	EGOTEA							
REF	VEND		IMACICE	DATE			BATCH	
NO.	NO.	NAME	DATE	WORKED		DESCRIPTION	NO.	TMUOMA
						•		
731549	CANTON DROP FORGE	, Wastewater						
0100	0 INVESTIGATION						-	
	9543 POSTAGE							
								_
	00052			9/19/97			105	1.24
					ACCOUNT	TOTAL		1.24
	9551 COPIER CHARG	TRS						
	7072 007241 4221							
	30270			9/19/97	COPIER	CHARGES	98	2.50
					ACCOUNT	TOTAL		2.50
			÷					
	9573 MICRO-COMPU	TER						
	25001			9/20/07	COMPUTE	না ন	260	10.00
	25001			6/23/31	ACCOUNT		200	10.00
					71000217			
					INVEST:	IGATION		13.74
					JOB 73:	1549 TOTAL		13.74
							•	
		•		TOTAL,	OTHER D	IRECT COSTS		13.74

REMIT PAYMENT TO: File 91849 Los Angeles, CA 90074-1849 Attn: Accounts Receivables

Street Address: 19101 VILLAVIEW ROAD, SUITE 301 CLEVELAND, OH!O 44119

Tel: (216) 486-9005 Fax: (216) 486-6119

INVOICE

2(b),3

AUGUST 8, 1997

CLIENT REF. :

INVOICE NO. :

00810971

PROJECT NO. :

731549-T1

CLIENT NO.

71275

TO: CANTON DROP FORGE, INC.

4575 SOUTHWAY STREET

CANTON, OHIO

44706

PLEASE REMIT TO:

PARSONS ENGINEERING SCIENCE, INC

FILE 91849

LOS ANGELES, CALIFORNIA

90074-1849

FOR: CANTON DROP FORGE, WASTEWATER RECYCLING

AUTHORIZATION: P.O. #98252 WBS 01000 - INVESTIGATION AMOUNT AUTHORIZED: \$7,000.00

ATTN: MR. KEITH HOUSEKNECHT

BILLING PERIOD: 6/28/97 THROUGH 7/25/97

CUF		=	ULATIVE-TO-DATE ROUGH 7/25/97
WBS 01000 - INVESTIGATION			41 006 26
DIRECT LABOR OH & PROFIT @1.95 X D.L.	\$.00 \$.00	52.6	\$1,896.26 \$3,697.71 \$203.23
ODCS WITHOUT HANDLING ODCS W/HANDLING Rate Markup: 5%	\$127.60 \$.00 \$.00		\$496.00 \$24.80
SUBTOTAL:	\$127.60		\$6,318.00
TOTAL THIS INVOICE:	\$127.60		\$6,318.00

PAGE: 1

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 7/25/97 BY WBS/COST CODE

 $g = g(x) \cdot g(x) = (x \cdot x) \cdot g(x \cdot x) = (1 - x) \cdot g(x) = (x \cdot x) \cdot g(x)$

INVOICE NO.: 00810971 PROJECT NO.: 731549-T1 CLIENT NO.: 71275

FORMAT NAME: SBLRFODC03

REF:

REFERENCE NUMBER	DESCRIPTION OF EXPENSES	TRUOMA
01000: INVESTIGATION		
9540	FREIGHT/EXPRESS/POSTAGE	112.08
9550	REPRODUCTION CHARGES	4.80
9560	COMMUNICATIONS	10.72
	127.60	
	GRAND TOTAL OTHER DIRECT COSTS	127.60

DETAIL OF OTHER DIRECT COSTS

FOR THE PERIOD ENDING 7/25/97
BY JOB/WBS/COST CODE

CLIENT REF.:

INVOICE NO.: 00810971
PROJECT NO.: 731549-T1
CLIENT NO.: 71275
FORMAT NAME: SBLRODCWTT

EQUIP/

	EQUIP/							
REF	VEND			INVOICE	DATE		BATCH	
NO.	NO.	NAME		DATE	WORKED	DESCRIPTION	ио.	AMOUNT
731549	CANTON	DROP FORGE, WASTEWATE	R					
0100	O INVES	STIGATION						
		•						
	9542 E	XPRESS						
06970573	O J2681	FEDERAL EXPRESS/U.S. (COLLECTIO	6/10/97			512	8.67
06970390	5 A4337	FEDERAL EXPRESS		5/23/97			387	51.41
06970390	5 A4337	FEDERAL EXPRESS		5/23/97			387	49.80
						ACCOUNT TOTAL		109.88
	9543 F	POSTAGE						
	00000					, DOGETAGE	486	. 32
	00052					POSTAGE	486	.78
	00052					POSTAGE	86	.78
	00052					POSTAGE	86	.32
	00052				7/18/9	7 POSTAGE ACCOUNT TOTAL	00	2.20
	9551	COPIER CHARGES						
	30270				6/20/9	7 COPIER CHARGES	93	1.40
	30270	1			6/20/9	7 COPIER CHARGES	93	.40
	30270	1			6/20/9	7 COPIER CHARGES	93	.60
	30270)			6/26/9	7 COPIER CHARGES	99	1.20
	30270)			7/18/9	7 COPIER CHARGES	94	1.20
						ACCOUNT TOTAL		4.60
	9561	TELEPHONE CHARGES						
	0005	1			6/20/	97 TELEPHONE CHARGES	102	1.82
	0005	1			6/20/	97 TELEPHONE CHARGES	102	- 44
	0005					97 TELEPHONE CHARGES	85	.43
	0005	1			7/18/	97 TELEPHONE CHARGES	96	1.03
						ACCOUNT TOTAL		3.72
•								
	9562	FAX CHARGES	•					
	0001	.5			6/13/	97 FAX CHARGES	81	3.00
		15				97 FAX CHARGES	81	4.00
			•			•		

DETAIL OF OTHER DIRECT COSTS
FOR THE PERIOD ENDING 7/25/97
BY JOB/WBS/COST CODE

CLIENT REF.:

INVOICE NO.: 00810971
PROJECT NO.: 731549-T1
CLIENT NO.: 71275
FORMAT NAME: SBLRODCWTT

EQUIP/

REF NO.	VEND NO.	NAME	INVOICE DATE	DATE WORKED	DESCRIPTION	BATCH NO.	AMOUNT
					ACCOUNT TOTAL		7.00
					INVESTIGATION		127,60
					JOB 731549 TOTAL		127.60
				TOTAL,	OTHER DIRECT COSTS		127.60

19101 Villaview Road, Suite 301 • Cleveland, Onio 44119 • (216) 486-9005 • Fax (216) 486-6119

PARESCL/597/Dec/EJK7-06

7 May 1997

26),7,1(c)

Mr. Keith Houseknecht Manager, Plant Engineering CANTON DROP FORGE, INC. 4575 Southway Street Canton, Ohio 44706

Subject:

Proposal to Provide Engineering Assistance Wastewater Recycling and/or Treatment

Dear Mr. Houseknecht:

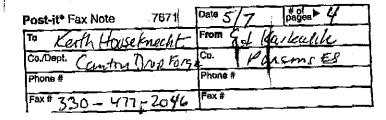
Subsequent to our meeting with you on 10 April 1997, and the several telephone conversations which we have completed in the interim, Parsons Engineering Science, Inc. (Parsons ES) understands that Canton Drop Forge, Inc. (CDF) is interested in receiving a proposal to address certain process water streams and their impacts on subsequent operations, current and potential discharge(s) to the public-owned treatment works (POTW), and the on-site Lagoon system. In developing this proposal, Parsons ES has considered the information provided during the previously described discussions as well as that contained in the Proposed Oily Process Wastewater and Steam Flow Diagram, as amended, and the list of process flows under consideration.

Specifically, CDF has indicated that a residual oily emulsion, which is generated when lubricating oil is injected into process steam used in the operation of the plant's steam hammers, has been observed in the low pressure steam/condensate manifold and may be creating adverse impacts (probable occurrence of foaming in the boilers, etc.), when the condensate stream is reused in subsequent operations. Additionally, subsequent to the hot process softener, lime precipitation appears to be occurring for a distance up to one (1) mile from the CDF discharge point into the sanitary sewer-line. As a consequence, the sewer district is eluctant to permit the discharge to continue and will likely be less receptive to a potential request from CDF to receive any additional streams (i.e., pretreated condensate).

OVERALL PROJECT APPROACH

Before the approach which best meets CDF's needs can be identified, an investigation is required to answer some important questions. Parsons ES can accomplish this investigation most efficiently with assistance, as needed, from CDF. Some key questions are listed below.

- 1. What are the potential re-uses of the identified process streams (i.e., condensate and hot process softener)? How much volume can be used at each process? What are the water quality requirements for each process stream?
- 2. What sources of process and/or wastewater are available for recycle? What are the volumes of each source? What is the quality of each stream? What pretreatment is required to meet the water quality requirements of each potential re-use application?



PARSONS

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Mr. Keith Houseknecht, Manager, Plant Engineering CANTON DROP FORGE, INC. 7 May 1997 Page 2 - Dec/EJK7-06

CDF has identified at least 13 possible sources and/or re-use applications, which were provided in a listing on 1 May 1997. The pretreatment required for each stream will vary based on the nature of the stream and the requirements of the recycled water user. It is Parsons ES' understanding that the least possible pretreatment, which will satisfactorily and consistently provide water for re-use in one of the prospective applications, is the ultimately desired result of this effort.

A combination of one or more operations may be appropriate. Likely candidate processes for addressing the condensate stream are (ultra)filtration, emulsion breaking, and oil removal. Other processes may be considered depending on the requirements to make a particular waste stream suitable for a particular reuse.

3. What are the potential volumes and qualities of process and/or wastewater to be discharged to the sewer or on-site Lagoon system? What are the pretreatment requirements for (continued) discharge to the sewer and POTW?

This question deals primarily with the existing discharge of the hot process softener stream to the sanitary sewer. Additionally, pretreatment requirements for discharge of the condensate stream to the sewer are contemplated.

PROPOSED SCOPE OF WORK

Parsons ES proposes to provide the services described in the following three tasks:

Task 1-Investigation/Evaluation Assistance

Parsons ES will review the existing sources of process and wastewater, the potential points of reuse, the pretreatment requirements for re-use and/or discharge to the sanitary sewer and potential alternatives for combining process and wastewater streams, as appropriate. The evaluation will also consider the potential disposition of any residuals which may be generated as a result of applying these alternatives. On-site data gathering efforts will be limited to a one-day effort involving two (2) Parsons ES personnel experienced in industrial process and wastewater treatment. During this exercise, the processes under consideration will be inspected, key operating personnel familiar with the issues will be interviewed, the previously referenced process flow diagram will be verified (for the purposes of this analysis only), process flow, pressure, temperature and quality data will be obtained for critical points in the CDF plant and samples will be collected from four (4) points for determination of water quality and pretreatment alternative feasibility. If additional sampling or other on-site activities are required, the level of effort and costs to complete same will be identified to CDF at that time.

Information on the following items will be collected during the one-day, on-site visit by Parsons ES personnel:

- Process water use and wastewater generation flow rates;
- Water quality requirements for boiler makeup and other identified candidate process streams;
- Process flow diagram revisions required to address the process and wastewater issues
 under consideration in this effort;

Mr. Keith Houseknecht, Manager, Plant Engineering CANTON DROP FORGE, INC. 7 May 1997 Page 3 - Dec/EJK7-06

- Available characterization information for each applicable process and wastewater stream;
- Description and application of current and planned process/wastewater treatment processes;
- · Description and status of discharges to the Lagoon system and sanitary sewer, and
- Other information critical to determining the feasibility of the recommended pretreatment options (e.g., spatial constraints).

Task 2-Treatability Testing and Analyses

Parsons ES will analyze key quality parameters (e.g., pH, total oil & grease, total dissolved solids) for each stream under consideration. Additionally, we will conduct treatability testing, either internally or in conjunction with appropriate equipment suppliers, on two (2) of the samples collected at the CDF plant to determine the most cost-effective approach(es) for achieving the required pretreatment levels for potential re-use applications and/or discharge. We will focus our attention on alternatives, such as ultrafiltration, which do not require significant operations and maintenance time, chemical additions, or cost impacts.

Task 3-Alternatives Development and Reporting

Based on the evaluations completed in Tasks I and 2, Parsons ES will identify several (up to three) potential alternatives for addressing the condensate and hot process softener stream issues. This evaluation will consider potential re-use of the process flows under evaluation through re-routing within the facility as well as pretreatment prior to discharge to the sanitary sewer. Screening factors used in this evaluation will include capital costs, O&M costs, availability, compatibility and spatial considerations (i.e., where will it fit). Simple block diagrams will be developed for each alternative showing the source flow rates, re-use flow rates, and the capacities of any storage vessels and/or sizes of any major treatment components, as appropriate. Budgetary cost estimates (+/-30%) will be identified for the proposed approaches.

Following completion of the alternatives evaluation, we will prepare a letter report summarizing the results of the work completed. The alternative(s) best meeting CDF's objectives will be recommended for CDF consideration and implementation. Equipment model numbers and costs for long-lead capital equipment, as appropriate, will be provided. Parsons ES will also provide an estimate for our design and implementation of the recommended approach(es) as a subsequent phase of this effort.

PROJECT TEAM

The Project Manager for the proposed project will be Michael R. Leffler, PE, Associate. Mr. Leffler has managed several similar studies for process re-use and pretreatment water re-use and/or discharge to POTW systems for other iron and steel fabrication mills and operations in the Northeast Ohio area. He will be assisted, as necessary, by Mr. Doug Morrison, during the Task I investigation and treatability studies, Mr. David G. Johnson, PE, as technical reviewer, and other Parsons ES staff, as necessary. Biographical data sheets are attached for the key project personnel.

PARSONS ENGINEERING SCIENCE, INC.

Mr. Keith Houseknecht, Manager, Plant Engineering
CANTON DROP FORGE, INC.

7 May 1997

7 May 1997 Page 4 - Dec/EJK7-06

SCHEDULE

It is estimated that this work can be completed within three weeks of authorization, assuming that appropriate assistance from vendors and suppliers of the targeted technologies is available on a highly responsive basis.

COMPENSATION

Parsons ES proposes to perform the services offered in this proposal on a "time and expenses, cost not-to-exceed" basis. Labor and expenses will be invoiced in accordance with the terms and conditions of our previously submitted (11 April 1997) Engineering Services Agreement (ESA). Parsons ES will not invoice CDF for more than \$7,000 without further authorization from CDF. This budget estimate assumes that the project can be initiated on or by 9 May 1997.

Our not-to-exceed amount is based on the following:

Task 1--20 hours of engineering plus support services, supplies, analyses and expenses

Task 2--20 hours of engineering plus support services and expenses

Task 3--15 hours of engineering plus support services and expenses

Should additional assistance be desired (e.g., engineering design or implementation of the selected alternative(s)), Parsons ES would be pleased to provide those services in accordance with the same schedule of compensation with an appropriate increase in the authorized not-to-exceed amount.

If this proposal is acceptable to you, please issue a purchase order referencing this proposal and our ESA. This will serve as our authorization to proceed. Thank you for the opportunity to present this proposal.

If you have any questions or wish to discuss the proposal, please do not hesitate to call either Mr. Leffler or Edward Karkalik at (216) 486-9005.

Very truly yours,

PARSONS ENGINEERING SCIENCE

Wilson H. Rownd, PE

Vice President/Manager

Michael R. Leffler, PE

Project Manager

WHR/MRL/dec Attachments cc: CMB (File) HPS BLOWDOWN

BOILER BLOWDOWN

SCRUBBER WATER

EXHAUST MANIFOLD SEPARATOR

HPS INLET SEPARATOR

STEAM HEATER CONDENSATE

COMPRESSOR COOLING WATER

RECTROURTING SYSTEM OVERFLOW

ANVIL HEATER LINE

LIME MIXING TANK DRAIN

POLYMEN TANK DRAIN

SCRUBBEN RECIRC TANK OVERFLOW

DOWATERING SLRUEN

2(%)

2(4)

HPS BLOWDOWN

BOILER BLOWDOWN

SCRUBBER WATER

EXHAUST MANIFOLD SEPARATOR

HPS INLET SEPARATOR

STEAM HEATER CONDENSATE

COMPRESSOR COOLING WATER

RECIRCULATING SYSTEM OVERFLOW

ANVIL HEATER LINE

LIME MIXING TANK DRAIN

POLYMEN TANK DRAIN

SCRUBBEN RECIRC TANK OVERFLOW

DOWATERING SCRUBN

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PARESCL/597/Dee/EJK7-06

RECEIVED

7 May 1997

MAY 12 1997

MATON DROP FORGE

Mr. Keith Houseknecht Manager, Plant Engineering CANTON DROP FORGE, INC. 4575 Southway Street Canton, Ohio 44706

Subject:

Proposal to Provide Engineering Assistance Wastewater Recycling and/or Treatment

Dear Mr. Houseknecht:

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Specifically, CDF has indicated that a residual oily emulsion, which is generated when lubricating oil is injected into process steam used in the operation of the plant's steam hammers, has been observed in the low pressure steam/condensate manifold and may be creating adverse impacts (probable occurrence of foaming in the boilers, etc.), when the condensate stream is reused in subsequent operations. Additionally, subsequent to the hot process softener, lime precipitation appears to be occurring for a distance up to one (1) mile from the CDF discharge point into the sanitary sewer-line. As a consequence, the sewer district is reluctant to permit the discharge to continue and will likely be less receptive to a potential request from CDF to receive any additional streams (i.e., pretreated condensate).

OVERALL PROJECT APPROACH

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PARSONS ENGINEERING SCIENCE, INC.

Mr. Keith Houseknecht, Manager, Plant Engineering CANTON DROP FORGE, INC. 7 May 1997 Page 2 - Dee/EJK7-06

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ANTON DROP FORGE

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Mr. Keith Houseknecht, Manager, Plant Engineering CANTON DROP FORGE, INC. 7 May 1997 Page 3 - Dee/EJK7-06

MAY 1 2 1997

ANTON DROP FORGE

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Mr. Keith Houseknecht, Manager, Plant Engineering CANTON DROP FORGE, INC. 7 May 1997 Page 4 - Dee/EJK7-06 RECEIVED

MAY 12 1997

ANTON DROP FORGE

SCHEDULE

It is estimated that this work can be completed within three weeks of authorization, assuming that appropriate assistance from vendors and suppliers of the targeted technologies is available on a highly responsive basis.

COMPENSATION

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Very truly yours,

PARSONS ENGINEERING SCIENCE

Wilson H. Rownd, PE

Vice President/Manager

Michael R. Leffler, PE

Project Manager

WHR/MRL/dee Attachments cc: CMB (File)

RECEIVED

MAY 12 1997

Biographical Data

DAVID G. JOHNSON

Environmental Engineer

ANTON DROP FORGE

EXPERIENCE SUMMARY

Management and technical direction of numerous hazardous and solid waste and industrial waste-water projects throughout the U.S. and abroad, with sixteen years of active professional practice. Major areas of expertise include industrial wastewater and groundwater treatment processes including biological treatment, carbon adsorption, air stripping, chemical precipitation, etc., as well as pollution prevention/waste minimization, storm water management, and hazardous waste site investigation and remediation.

EXPERIENCE RECORD

1980-Date

Parsons Engineering-Science. Office Manager (1995-Date); Technical and administrative management of 90 engineers, geologists, scientists, and support personnel. Projects include RCRA/CERCLA studies and remedial designs, site investigations, RI/FS, AST/UST tank removal and remedial projects, industrial wastewater studies and design, pollution prevention, air, wastewater, and hazardous waste permitting, and other environmental projects.

Engineering Technical Manager (1993-1995); Manager, Industrial Waste Group (1986-1993); Manager, Environmental Studies Group (1985-1986); Project Manager (1980-1985). Management and technical direction of wastewater, hazardous waste, and other environmental assessments, studies and design projects for numerous industrial and governmental clients, including clients in the petroleum refining, petrochemical, chemical, pharmaceutical, metals processing, transportation, food processing, regional waste treatment, semiconductor, and electronics industries, among others. Conducted environmental Phase I assessments and audits of numerous industrial facilities covering the areas of PCBs, water, wastewater, asbestos, air, and solid and hazardous waste. Conducted audits of municipal and industrial wastewater treatment systems for EPA Region VI. Technical direction of pollution prevention/waste minimization projects, including development of BMP and Stormwater Pollution Prevention (SWPPP) Plans. Stormwater sampling, analysis, and permitting. Conducted bench-scale chemical and biological treatability studies on coal gasification, petroleum refining, petrochemical, aluminum processing, and other industrial wastewaters, involving biological treatment, carbon adsorption, air stripping, oil/water separation, chemical precipitation, chemical oxidation, and other unit processes. Evaluated existing industrial wastewater treatment facilities, and prepared conceptual wastewater treatment system designs for petroleum refining, petrochemical, aluminum manufacturing and other facilities. Managed a project to investigate the feasibility of thermal enhancement of soil vapor extraction for remediation of contaminated soils at a New Jersey chemical facility. Managed design of sludge handling equipment for several industrial facilities. Provided sampling and permit assistance to industrial clients for new and modified water, wastewater, stormwater, and/or hazardous waste permits. Prepared environmental assessments for several major projects, including a major airport expansion and a new Central Florida phosphate mine.

MAY 12 1997

DAVID G. JOHNSON Environmental Engineer Page 2 ANTON DROP FORGE

Managed several major solid and hazardous waste projects, including several RCRA and CERCLA projects to conduct preliminary site assessments and site inspection activities at over 1,500 potential hazardous waste sites in Texas. Managed projects to conduct investigations of 20 hazardous waste sites and 13 sanitary, construction and demolition, and sludge landfills in New York State. Managed RI/FS activities at a former specialty chemical facility in New Jersey, including a pilot-scale soil vapor extraction (SVE) study, and a wellfield contaminated with TCE in New York State. Managed a project to assess the feasibility of the use of thermal enhancement of SVE at a New Jersey chemical facility. Also managed a project to conduct solid waste disposal facility inspections at 257 industrial facilities.

Conducted Phase 1 Installation Restoration Program projects at four Air Force bases and a Phase II investigation at Westover AFB, MA for the Department of Defense to identify practices potentially resulting in groundwater contamination and contaminant migration, including ranking of identified sites for further investigations. Prepared hazardous waste management plans to meet RCRA requirements for several refineries and petrochemical plants in Texas, Louisiana, and New Mexico. Evaluated fly ash handling alternatives and coal pile runoff for an industrial complex in Portugal. Managed a project to evaluate sludge handling alternatives for a regional industrial wastewater treatment plant. Managed projects evaluating potential groundwater contamination for several refinery and other manufacturing facilities. Provided evaluation and coordination of major hydrocarbon recovery program involving over 70 recovery wells, 250 observation wells, and recovered groundwater treatment.

- 1978-1980 Espey, Huston & Associates, Inc., Houston, Texas. Staff Engineer I. Preparation of federal flood insurance studies for 13 coastal communities and 4 counties in Texas. Responsible for the data collection, hydrologic, and hydraulic analyses using the computer program HEC-2, and report writing, as well as coordination of staff engineers and technicians involved in the project. Designed drainage ditch improvements for several Gulf Coast communities.
- 1977-1978 University of Texas, Austin, Texas, Dept. of Engineering (Environmental Health).

 Research Assistant II. Performed literature review and analysis of data pertaining to the sources and influx of nitrogen species into confined aquifers, and the fate of ammonia used for in situ uranium solution mining.
- 1976-1977 University of Texas, Austin, Texas, Dept. of Civil Engineering. Research Assistant II. Performed data reduction and analysis and application of computer models to predict dynamic wheel loadings on pavements and bridges.

EDUCATION

B.S. in Civil Engineering with Highest Honors, 1977, University of Texas, Austin, Texas M.S. in Engineering (Environmental Health), 1979, University of Texas, Austin, Texas

PROFESSIONAL AFFILIATIONS

Registered Professional Engineer (New York, 1987, No. 064133) Water Environment Federation TAPPI

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MAY 1 2 1997

LANTON DROP FORGE

DAVID G. JOHNSON Environmental Engineer Page 3

PUBLICATIONS

"Literature Review and Preliminary Analysis of Inorganic Ammonia Pertinent to South Texas In-Situ Leaching," with others. Center for Research in Water Resources Report No. CRWR-155, EHE 78-01, 1978.

"Investigation of the Fate of Ammonia From In-Situ Uranium Solution Mining," with others. Technical Report EHE 79-01, 1979.

"RCRA 3012 and Superfund Enforcement at the State Level," with others. In Management of Uncontrolled Hazardous Waste Sites, Fifth National Conference, November 1984.

"Cost Model for Selected Technologies for Removal of Gasoline Components in Groundwater", American Petroleum Institute (API) Publication 4422, February 1986.

PAPERS AND PRESENTATIONS

"Nitrification and In-Situ Uranium Solution Mining," presented at the 1979 SPE Annual Technical Conference and Exhibition, September 1979, and at the Texas Section ASCE Fall 1979 meeting, October 1979, at College Station (coauthor M. Humenick).

"Industrial Wastewater Pretreatment: History, Status, and Outlook," presented at the Mohawk Valley Environmental Information Exchange, May 1993.

MAY 12 1997

ANTON DROP FORGE

Biographical Data

MICHAEL R. LEFFLER

Chemical/Environmental Engineer

EXPERIENCE SUMMARY

Extensive experience in environmental studies and permitting, wastewater treatment plant design and operations, and other engineering studies for both industrial and municipal clients.

EXPERIENCE RECORD

1974-Date

Parsons Engineering Science (Parsons ES). Project Manager (1979-Date). Engineering Department Manager (1991-1993); Department Head; Industrial Wastes, Plant Operations and Environmental Studies (1988-1990). Coordinated all activities of the Parsons ES Cleveland Engineering Department and Industrial Wastes, Plant Operations and Environmental Studies Group, respectively.

Conducted wet weather bypass investigation for 22.5 mgd municipal wastewater treatment plant and collection system. Work included evaluation of alternatives to eliminate bypassing and the impact of blending waste streams on the final effluent. Prepared a Satellite Sewer Discharge Control Program for imposing NPDES requirements on customer cities.

Assisted in Comprehensive Evaluation of Combined Sewer System for a large city to determine methods to eliminate capacity problems.

Prepared preliminary design and cost estimates for wastewater treatment systems for two major organic chemical manufacturing facilities. Estimates were prepared for two systems at each location and included biological treatment, chemical oxidation, steam stripping, and sand filtration.

Evaluated existing system, designed modifications and provides ongoing operations assistance for a package extended aerative wastewater treatment systems.

Evaluated the need and options for wastewater pretreatment system at a steel rolling mill, designed system modifications, prepared permit to install and indirect discharge permit applications, assisted in securing EPA permits, and assisted as startup and initial operation of the system. Treatment included oil and grease removal.

Supervised sewer flow metering at 19 locations for one month and utilized data to allocate the operating costs of a wastewater treatment plant among four municipalities.

Supervised field location of approximately 25,000 feet of potable water lines and appurtenances on a college campus and preparation of AutoCad drawings for use in a GIS System.

Performed comprehensive studies for industrial client to identify and correct sources of non-compliant discharges under stormwater NPDES permit and municipality issued industrial pretreatment permit. Work included evaluations and optimization assistance for a 25 gpm chrome reduction/metals removal system.

Supervised treatability testing and design of emulsified oil removal system for an industrial client.

MICHAEL R. LEFFLER Chemical/Environmental Engineer Page 2

MAY 1 2 1997

SANTON DROP FORGE

Served as Project Manager for design of modifications to convert an aerated lagoon treatment system to an activated sludge system with recycle for an industrial facility, prepared permit to install application, prepared Operating Guide, provided operator training and supervised startup of the modified facility.

Supervised operation of a 22.5 mgd wastewater treatment plant with fixed film biological reactors under a 10-year operations contract.

Developed computerized data management system for a 22.5 mgd municipal wastewater treatment facility.

Supervised preparation of Oil Spill Prevention and Countermeasure Plans (SPCC) for five roofing products manufacturing facilities and three specialty steel mills.

Served as Project Manager for design of a 300 gpm metals removal facility to remove arsenic and hexavalent chromium from landfill leachate.

Designed piping and control systems for recovering hydrocarbons from soil by vapor extraction and assisted in data analysis for operating system.

Performed evaluation and designed modifications to a 13 mgd plant water pumping system for a large industrial facility to accommodate aggressive water use reduction program.

Conducted testing and evaluation of an industrial fume scrubber for acid fumes.

Supervised start-up, provided operations assistance, developed operator training program, and implemented maintenance schedules and records management system for a 50 mgd physical/chemical wastewater treatment plant and 300 mgd Combined Sewer Overflow (CSO) Treatment Facility; wastewater treatment processes included lime precipitation, recarbonation, pressure filtration, carbon adsorption, disinfection, centrifuge sludge dewatering and incineration; CSO treatment included screening and sedimentation with up to 6 million gallons storage capacity. Work included preparation of applications for permit to operate, negotiation of applicable air pollution limits, and coordination of stack testing for two incinerators.

Responsible for preparation of Operation and Maintenance (O&M) Manuals for a 66 mgd wastewater pumping station including an odor control system utilizing ozone, two industrial facilities and a hazardous waste incineration system. Served as technical director for preparation of O&M Manual for a sludge composting facility and a 33 mgd, two-stage biological treatment plant. Supervised preparation of O&M Manuals, Start-up and Operator Training at a 12 mgd activated sludge plant and two wastewater treatment plants using fixed film biological reactors with capacities of 35 and 45 mgd.

Project Engineer (1974-1979). Responsible for systems specification writing, design and operations reviews, plant start-up, and troubleshooting for advanced wastewater treatment facilities. Designed chemical feed systems for an industrial waste treatment facility. Conducted a feasibility study on use of chlorinated industrial waste in domestic wastewater treatment. Conducted an odor investigation at a river dredging disposal site. Work included air sampling, odor quantification using an odor panel and sulfur determination using a sulfur chromatograph. Prepared oil Spill Prevention and Countermeasure Plan (SPCC) for an automotive equipment manufacturing complex.



MICHAEL R. LEFFLER Chemical/Environmental Engineer Page 3

MAY 1 2 199

ANTON DROP FORGE

Directed start-up of centrifuge sludge dewatering system, developed a staffing plan, and prepared an O&M Manual for a 50 mgd physical/chemical wastewater treatment plant. Involved in start-up and O&M Manual preparation for a 4 mgd pure oxygen activated sludge plant with tertiary treatment. Evaluated operations of sludge handling facilities at a 25 mgd municipal wastewater treatment plant.

1972-1974 Havens and Emerson, Ltd., Cleveland, Ohio. Project Engineer. Project Engineer responsible for the design of phosphorus removal facilities, chemical storage and handling systems, polymer feed system, and pH adjustment system including associated tanks, buildings and appurtenances for an existing 12 mgd activated sludge treatment facility. Staff Engineer on various aspects of design of a 22 mgd pure oxygen activated sludge wastewater treatment plant. Responsibilities included chemical handling systems, grit removal, and complete checking of plant hydraulics.

EDUCATION

B.S. Engineering (Environmental), 1972, Purdue University, West Lafayette, Indiana M.S. Chemical Engineering, 1977, Cleveland State University, Cleveland, Ohio

PROFESSIONAL AFFILIATIONS

Registered Professional Engineer (Ohio 1977, No. E-41889)
Certified Class III Wastewater Works Operator (Ohio 1981, No. 3-81-53)
American Academy of Environmental Engineers (Diplomate)
American Institute of Chemical Engineers
Water Environment Federation

PAPERS AND PRESENTATIONS

"Computer Control of a Physical-Chemical Treatment Plant", presented at the Fifty-Ninth Annual Meeting of the Ohio Water Pollution Control Conference, June 1985 (co-authors: L. Debevec and T. P. Meister)

MAY 12 1997

MANTON DROP FORGE

Biographical Data

DOUGLAS A. MORRISON

Chemical/Environmental Engineer

EXPERIENCE SUMMARY

Project manager/project engineer with experience in the treatment of industrial solid and liquid wastes. Experienced in conceptual design, biological and physical/chemical treatability studies, feasibility studies, detailed design for wastewater, groundwater, and leachate treatment systems and providing air engineering services. Experienced in the conduct of pollution prevention/waste minimization studies for various industrial and federal clients.

EXPERIENCE RECORD

1991-Date Parsons Engineering Science. Environmental/Chemical Engineer.

Detailed Design (Typical Projects):

Provided detailed design and specifications package for an oil/water separation system for treating storm water runoff at a vehicle maintenance facility for a major interstate busing company.

Served as a project engineer on the closure design of a 60-acre municipal landfill. The design included waste consolidation, a multi-layered low permeability cap, a leachate collection system, and a trench gas venting system.

Provided detailed design and specifications package for a groundwater/leachate collection and treatment system. System components include equalization, pH neutralization, and multi-media sand filtration.

Treatability Studies (Typical Projects):

Organized and conducted an extensive battery of studies for the treatment of pharmaceutical wastewaters. Bench-scale studies conducted included anaerobic digestion of waste activated sludge (WAS) and mycelial solids, aerobic digestion of WAS and mycelial solids, lime stabilization of digested solids, serum bottle anaerobic toxicity assessments of process wastewaters/solvents, batch nitrification inhibition studies of process wastewaters/solvents, and sludge conditioning of WAS generated from treatment of pharmaceutical wastewaters. Coauthored the technical reports detailing the results of these studies.

Supervised the operation of an alkaline hydrolysis pilot-scale treatability study for the destruction of iron-complexed cyanide leachate. Coauthored the technical report detailing the results of this study.

Organized and conducted a battery of aerobic digestion studies on WAS generated in the treatment of baby food manufacturing wastewaters. Study determined anticipated kinetic coefficients and temperature dependency which was utilized in the detailed design of full-scale solids handling facilities.



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DOUGLAS A. MORRISON Chemical/Environmental Engineer Page 2

ANTON DROP FORGE

Feasibility Studies (Typical Projects):

Conducted a feasibility study for the remediation of a State Superfund Site containing soils and building surfaces contaminated with PCBs and heavy metals.

Assisted in a feasibility study for the remediation of an operating jet fuel distribution facility contaminated with JP-4 and creosols.

Prepared a feasibility study for the remediation of a State Superfund Site consisting of a landfill containing municipal/industrial refuse. The recommended alternative, which received state approval, included a Part 360 Cap with no provisions/requirements for groundwater remediation.

Assisted in the preparation of a feasibility study for a 70 acre USEPA superfund site highly contaminated with lead. Efforts included developing remedial alternatives and preparing detailed remedial cost estimates.

Conceptual Design (Typical Projects):

Assisted in the preparation of conceptual design reports for the treatment of complex wastewater discharges for pharmaceutical manufacturing firms located in Pennsylvania, New Jersey and New York. Efforts included wastewater sampling/characterization, review of potential management/treatment technologies, and the development of process trains which would provide adequate treatment of these discharges.

Have provided conceptual designs for numerous facilities for groundwater, leachate, and process wastewater recovery and treatment. A conceptual design for a "zero discharge" pressure washing system has been incorporated in over 100 facilities for a nation-wide truck engine repair corporation.

Pollution Prevention/Waste Minimization (Typical Projects):

Coauthored a waste minimization report for a Fortune 100 metal fabricating/printed circuit board manufacturer. Report included a review of innovative technologies, alternative processes, safe substitutes, as well as recommended process modifications to reduce waste stream toxicity/volume.

Prepared a Pollution Prevention Opportunity Assessment for a phenolic resin formulating/fabrication facility. The report concentrated on the facility's hazardous waste streams; however solid waste reduction measures were also evaluated. Detailed recommendations, including an economic feasibility analysis, were developed which formulated a pollution prevention implementation strategy.

Assisted in the preparation of a Pollution Prevention Opportunity Assessment for a U.S. Army post (Fort Drum, New York). Primary work efforts included obtaining process data and accurate waste generation information for the post and completing the economic analysis for the P2 opportunity assessment. Economic analyses (including sensitivity analysis) were conducted for 49 pollution prevention alternatives.

Assisted in the preparation of an annual update for a Hazardous Waste Reduction Plan (HWRP) for a master aluminum production facility.

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DOUGLAS A. MORRISON Chemical/Environmental Engineer Page 3

JANTON DROP FORGA

Facility Prevention Plans (Typical Projects):

Have prepared/managed a variety of facility prevention plans including: Spill Prevention, Control and Countermeasures plans (SPCCs), Storm Water Pollution Prevention plans (SWPPPs), Best Management Practices plans (BMPs), Chemical Bulk Storage Spill Prevention Reports (CBS SPRs), Facility Response Plans (FRPs), Process Safety Management plans (PSMs), and New York State Contingency Plans (required for large-quantity generators).

Responsible for managing storm water compliance for a major interstate busing company which has seeked coverage under a USEPA group permit. Have managed the preparation of notice of intents (NOIs) and SWPPPs for eighteen (18) facilities located in twelve (12) states who currently do not recognize USEPA group permits.

Project Manager for preparation of site-specific SPCCs for thirteen (13) locations for a major interstate busing company. Have managed professional engineers in eight separate ES offices to complete SPCC preparation/SPCC 3-year update projects in a timely, cost-effective manner. Project engineer in the preparation of two SPCC plans for a major New York State utility.

Air Engineering Services (Typical Projects):

Experienced in many facets of air-related projects and services including the preparation of emission estimate calculations, air permitting, RACT evaluations, and design/evaluation of air pollution abatement/control devices.

Have prepared calculations for volatile organic compounds (VOCs) emissions from eight (8) bulk petroleum storage terminals located in New York and Pennsylvania. Have calculated NOx, VOCs, and particulate emission estimates for two bus maintenance facilities.

Completed air permits and have advised in air permit submittals in New York State, Massachusetts, California, and Virginia. Prepared an air permit submittal to operate a remedial treatment system at an Air Force facility located in New York State.

Have assisted in the preparation of a RACT evaluation for a pharmaceutical firm located in New Jersey. The evaluation addressed the utilization of isopropanol as a carrier solvent and bulk disinfectant in facility operations.

1990-1991 Clarkson University. Research Assistant. "The Fate and Effects of Photoprocessing Effluents in Conventional Biological Treatment". A research project funded by Eastman Kodak Company. Studied the effects of photoprocessing effluents on the activated sludge process using continuous-flow and fill-and-draw bench-scale reactors.

EDUCATION

- B.S., Chemical Engineering, 1990, Clarkson University, Potsdam, New York
- M.S., Environmental Engineering, 1992, Clarkson University, Potsdam, New York
- M.S. Thesis Title "The Fate and Effects of Photoprocessing Effluents on the Activated Sludge Process."

MORRISDA/091/0295#



MAY 12 1997

SANTON DROP FORGE

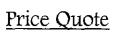
DOUGLAS A. MORRISON Chemical/Environmental Engineer Page 4

PROFESSIONAL AFFILIATIONS

New York Water Pollution Control Federation - Member

PUBLICATIONS AND PRESENTATIONS

- "Pilot-Study of Iron Complexed Cyanide Treatment by Alkaline Hydrolysis", presented at the Water Environment Federation Conference, Chicago, IL, 1994 (coauthors J.L. Swanger and M.B. Fox).
- "Response of Continuous-Flow Activated Sludge Reactors to Photoprocessing Wastewaters," Water Research, May/June 1994 (coauthor S. G. Pavlostathis).
- "Aerobic Biodegration Potential of Photoprocessing Wastewaters," published in Water Environment Research, May 1993 (coauthor S. G. Pavlostathis).
- "Aerobic Treatment of Photoprocessing Effluents," published in the proceedings for the 23rd Mid-Atlantic Industrial Waste Conference, University of Pittsburgh, 1991 (coauthors S. G. Pavlostathis and K. Sridhar).
- "Aerobic Treatment of Photoprocessing Effluents," presented at the Environmental Science and Engineering Research Seminar, 1991.



2(6)

Date: May 27, 1997

Canton Drop Fordge

	PRODUCT CODE	PACKAGE	\$/GAL QI	UANTITY DELIVERY LOCATION
Rando HD 150	1660	Tote	\$2.20/gal	Canton. OH
Vanguard 680*	631	Drums	\$3.42/gal	Canton, OH

^{*}Vanguard 680 priced in drums but delivered in totes.

No Drum or Pallet Charges

Terms

NET 60 Days

Thomas G. Hach Senior Sales Engineer



VANGUARD

Code 620 Vanguard 460 Code 631 Vanguard 680 Code 624 Vanguard 1000

Vanguard oils are premium steam cylinder oils and worm gear lubricants.

Product Application

Vanguard oils are recommended for lubrication of steam cylinders under dry or wet conditions and where exhaust steam is used. They are also suitable for lubricating worm gear drives, low speed heavily-loaded gears, and low-speed and high temperature bearings. Vanguard oils possess excellent lubricity and wetability characteristics along with high VI, foam resistance and rust protection properties. These oils are compounded lubricants containing a stable fatty additive. In addition to possessing the ease of atomization and wetability required for effective steam engine lubrication, they separate readily from steam condensate.

Product Description and Features

Vanguard oils are available in three viscosity grades; ISO 460, 680 and 1000. They are compounded with a refined grade of acidless tallow which allows them to separate easily from condensate and provide good heat resistance. These oils tend to form emulsions when exposed to water and/or steam; however, they will separate water more readily than products containing many other types of fatty materials. Vanguard oils are particularly suited for use with higher pressure and lower water content steam. Other features of Vanguard oils are good atomizing properties and the ability to bling to cylinder parts.

Benefits

In service Vanguard provides:

- Excellent lubrication of steam cylinders
- Protection where steam condensate presents a problem
- · Excellent film strength to protect worm gears
- Protects yellow metals

Product Recommendations and Approvals

Vanguard oils are recommended for use as steam cylinder lubricants and worm gear lubricants. The Vanguard series fully meets the requirements of AGMA Standard 250.04 Specification "Lubrication of Industrial Enclosed Gear Drives".

(Issued 4-95)

Product Maintenance

Following the maintenance practices as specified by the OEM's will help maximize equipment life. The service life of **Vanguard** oils are dependent on many variables. Serious contamination from external sources such as solid particles, water (in the case of enclosed gear lubrication) or other fluids call for immediate corrective action. As is always the case, it is important to follow the manufacturers' recommendations regarding equipment and lubricant maintenance.

Typical Characteristics

Vanguard		460	680	1000
Code No.		620	631	624
Appearance		D	ark Red	
AGMA No.		7	8	
	Test Method			
Gravity. API	D 287	24.9	23.0	21.7
Flash, COC,°F	D 92	455	545	500
Pour Point, °F	D 97	+10	+20	40
Viscosity				
cSt at 40°C	D 445	455	6 59	930
cSt at 100°C	D 445	30.4	36.5	47.9
SUS at 100°F	(calc)	2438	3569	5050
SUS at 210°F	(calc)	147	178	233
Viscosity Index	D 2270	96	90;	96
Carbon Residue, wt%	D 189	0.80	1.3	0.94
Fatty Oil, wt%	D 94	4.5	5.6	5.7

Handling Practices

For information on the safe handling and use of these products, refer to their Material Safety Data Sheets. For more information and availability, call 1+800-STAR-TLC.

Date Issued: 05-02-96 Supersedes: 12-08-95

61789-97-7 3.00-9.99

N.T. - NOT TESTED

TEXAC0 MATERIAL SAFETY DATA SHEET

NOTE: Read and understand Material Safety Data Sheet before handling or disposing of product.

1. CHEMICAL PRODUCT AND COMPANY IDENTIFICATION

MATERIAL IDENTITY

Product Code and Name:

00631 VANGUARD 680

Chemical Name and/or Family or Description:

Cylinder & Valve Dils

Manufacturer's Name and Address:

TEXACO LUBRICANTS COMPANY

A DIVISION OF TEXACO REFINING AND MARKETING INC.

P.O. Box 4427

Houston, TX 77210-4427

Telephone Numbers:

Transportation Emergency-Company : (914) 831-3400

CHEMTRES : (800) 424-9300

Health Emergency -Company : (914) 831-3400

General MSDS Assistance : (914) 838-7204 : (914) 838-7336 Technical Information -Fuels

-Chemical : (512) 459-6543 -Lubricant/: (800) 782-7852

Antifreezes

-Additives : (713) 235-6278 -\$olvents ; (800) 876-3738

2. COMPOSITION/INFORMATION ON INGREDIENTS

THE CRITERIA FOR LISTING COMPONENTS IN THE COMPOSITION SECTION IS AS FOLLOWS: CARCINOGENS ARE LISTED WHEN PRESENT AT O.1 % OR GREATER, COMPONENTS WHICH ARE OTHERWISE HAZARDOUS ACCORDING TO OSHA ARE LISTED WHEN PRESENT AT 1.0 % OR GREATER: NON-HAZARDOUS COMPONENTS ARE LISTED AT 3.0 % OR GREATER. THIS IS NOT INTENDED TO BE A COMPLETE COMPOSITIONAL DISCLOSURE. REFER TO SECTION 14 FOR APPLICABLE STATES' RIGHT TO KNOW AND OTHER REGULATORY INFORMATION.

Product and/or Component(s) Carcinogenic According to:

IARC DSHA NTP ÖTHER NONE

Composition: (Sequence Number and Chemical Name)

Seq. Chemical Name CAS Number Range in %

O1 # Solvent deasphalted residual petroleum oil

64741-95-3 65.00-79.99 64742-65-0 20.00-34.99 02 # Solvent-dewaxed heavy paraffinic petroleum

distillates

PRODUCT IS NON-HAZARDOUS ACCORDING TO OSHA (1910.1200).

* COMPONENT IS HAZARDOUS ACCORDING TO OSHA.

F COMPONENT, BY DEFINITION, IS CONSIDERED HAZARDOUS ACCORDING TO OSHA BECAUSE IT CARRIES THE PERMISSIBLE EXPOSURE LIMIT (PEL) FOR MINERAL OIL MIST.

Exposure Limits referenced by Sequence Number in the Composition Section

Seq. Limit

01 5 mg/m3 TWA-OSHA (MINERAL OIL MIST)

01 mg/m3 TWA-ACGIH (MINERAL OIL MIST) mg/m3 STEL ACGIH (MINERAL OIL MIST) 01 10

02 5 mg/m3 TWA-QSHA (MINERAL OIL MIST)

02 mg/m3 TWA-ACGIH (MINERAL DIL MIST) 5

mg/m3 STEL ACGIH (MINERAL DIL MIST) 02 10

3. HAZARD IDENTIFICATION

03 * Acidless tallow oi?

EMERGENCY OVERVIEW

Appearance:

Dark red liquid

Odor:

Not determined

PAGE: N.D. - NOT DETERMINED N.A. - NOT APPLICABLE

- LESS THAN

- GREATER THAN

PRODUCT CODE: 00631 NAME: VANGUARD 680

Date Issued: 05-02-96 Supersedes: 12-08-95

3. HAZARD IDENTIFICATION (CONT)

WARNING STATEMENT

NONE CONSIDERED NECESSARY

Health:

NFPA

Health: Flammability: 1 Reactivity: 0 Special

Flammability: 1

Reactivity: 0

Special

POTENTIAL HEALTH EFFECTS

EYE SKIN INHALATION

INGESTION

Primary Route of Exposure: X

<u>X</u>

X

EFFECTS OF OVEREXPOSURE

Eves:

May cause minimal irritation, experienced as temporary discomfort.

Skin:

Brief contact is not irritating. Prolonged contact, as with clothing wetted with material, may cause defatting of skin or invitation, seen as local redness with possible mild discomfort.

Other than the potential skin irritation effects noted above, acute (short term) adverse effects are not expected from brief skin contact; see other effects, below, and Section 11 for information regarding potential long term effects.

Inhalation:

Vapors or mist, in excess of permissible concentrations, or in unusually high concentrations generated from spraying, heating the material or as from exposure in poorly ventilated areas or confined spaces, may cause irritation of the nose and throat, headache, nausea, and drowsiness.

Ingestion:

If more than several mouthfuls are swallowed, abdominal discomfort, nausea, and diarrhea may occur.

Sensitization Properties:

Unknown.

Chronic:

No adverse effects have been documented in humans as a result of chronic exposure. Section 11 may contain applicable animal data.

Medical Conditions Aggravated by Exposure:

Because of its defatting properties, prolonged and repeated skin contact may aggravate an existing dermatitis (skin condition).

Other Remarks:

None

4. FIRST AID MEASURES

Eves:

Flush eyes with plenty of water for several minutes. Get medical attention if eye irritation persists.

Wash skin with plenty of soap and water for several minutes. Get medical attention if skin irritation develops or persists.

If more than several mouthfuls of this material are swallowed, give two glasses of water (16 oz.). Get medical attention.

Inhalation:

If irritation, headache, nausea, or drowsiness occurs, remove to fresh air. Get medical attention if breathing becomes difficult or respiratory irritation persists.

> PAGE: 2



4. FIRST AID MEASURES (CONT)

Other Instructions:

Remove and dry-clean or launder clothing soaked or soiled with this material before reuse. Dry cleaning of contaminated clothing may be more effective than normal laundering. Inform individuals responsible for cleaning of potential hazards associated with handling contaminated clothing.

5. FIRE-FIGHTING MEASURES

Ignition Temperature - AIT (degrees F):

Not determined.

Flash Point (degrees F):

530 (COC)

Flammable Limits (%):

Lower: Not determined. Upper: Not determined.

Recommended Fire Extinguishing Agents And Special Procedures:

Use water spray, dry chemical, foam, or carpon dioxide to extinguish flames. Use water spray to cool fire-exposed containers. Water or foam may cause frothing.

Unusual or Explosive Hazards:

None

Special Protective Equipment for Firefighters:

No special equipment or procedures required.

6. ACCIDENTAL RELEASE MEASURES (Transportation Spills: CHEMTREC (800)424-9300)

Procedures in Case of Accidental Release, Breakage or Leakage:

Ventilate area. Avoid breathing vapor. Wear appropriate personal protective equipment, including appropriate respiratory protection. Contain spill if possible. Wipe up or absorb on suitable material and shovel up. Prevent entry into sewers and waterways. Avoid contact with skin, eyes or clothing.

7. HANDLING AND STORAGE

Precautions to be Taken in

Handling:

Minimum feasible handling temperatures should be maintained.

Storage:

Periods of exposure to high temperatures should be minimized. Water contamination should be avoided.

8. EXPOSURE CONTROLS/PERSONAL PROTECTION

Protective Equipment (Type)

Eve/Face Protection:

Safety glasses, chemical type goggles, or face shield recommended to prevent eye contact.

Skin Protection:

Workers should wash exposed skin several times daily with soap and water. Soiled work clothing should be laundered or dry-cleaned.

Respiratory Protection:

Airborne concentrations should be kept to lowest levels possible. If vapor, mist or dust is generated and the occupational exposure limit of the product, or any component of the product, is exceeded, use appropriate NIOSH or MSHA approved air purifying or air supplied respirator after determining the airborne concentration of the contaminant. Air supplied respirators should always be worn when airborne concentration of the contaminant or oxygen content is unknown.

Ventilation:

Adequate to meet component occupational exposure limits (see Section 2).

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Date Issued: 05-02-96 Supersedes: 12-08-95



8. EXPOSURE CONTROLS/PERSONAL PROTECTION (CONT)

Exposure Limit for Total Product:

None established for product; refer to Section 2 for component exposure limits.

9. PHYSICAL AND CHEMICAL PROPERTIES

Appearance:

Dark red liquid

Odor:

Not determined

Boiling Point (degrees F):

Not determined.

Melting/Freezing point (degrees F):

Not applicable.

Specific Gravity (water=1):

.9188

pH of undiluted product:

Not applicable.

Vapor Pressure:

Not determined

Viscosity:

670 cSt at 40.0 C

VOC Content:

Not determined.

Vapor Density (air=1):

Not determined.

Solubility in Water (%):

Not determined.

Other: None

10. STABILITY AND REACTIVITY

This Material Reacts Violently With:

(If Others is checked below, see comments for details)

Air Water Heat Strong Oxidizers Others None of These

.

Comments:

None

Products Evolved When Subjected to Heat or Combustion:

Toxic levels of carbon monoxide, carbon dioxide, irritating aldehydes and ketones.

Hazardous Polymerizations: DO NOT OCCUR

11. TOXICOLOGICAL INFORMATION

TOXICOLOGICAL INFORMATION(ANIMAL TOXICITY DATA)

Median Lethal Dose

Oral:

LD50 Believed to be > 5.00 g/kg (rat) practically non-toxic

Inhalation:

Not determined.

Dermal:

LD50 Believed to be > 2.00 g/kg (rabbit) practically non-toxic

Irritation Index, Estimation of Irritation (Species)

Skin:

(Draize) Believed to be < .50 /8.0 (rabbit) no appreciable effect

Eyes:

(Draize) Believed to be < 15.00 /110 (rabbit) no appreciable effect

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AME: VANGUARD 680	Supersedes:	12-08-95
1. TOXICOLOGICAL INFORMATION (CONT)	·	··-
Sensitization: Not determined: Other: None		
2. DISPOSAL CONSIDERATIONS		
Waste Disposal Methods		
This product has been evaluated for RCRA characteris the criteria of a hazardous waste if discarded in it Under RCRA, it is the responsibility of the user of mine at the time of disposal, whether the product me hazardous waste. This is because product uses, trar processes, etc. may render the resulting materials has a superior of the resulting materials for the re	s purchased for the product to ets RCRA criter asformations, m	rm. deter- ria for
Remarks None		
3. TRANSPORT INFORMATION		
Transportation DOT: Proper Shipping Name: Not regulated		
IMDG: Proper Shipping Name: Not evaluated		
ICAD: Proper Shipping Name: Not evaluated		
TDG: Proper Shipping Name: Not evaluated		
14. REGULATORY INFORMATION		
Federal Regulations: SARA Title III: Section 302/304 Extremely Hazardous Substances		
	CAS Number	Range in %
Section 302/304 Extremely Hazardous Substances (CO Seq. TPO RC None	NT)	
Section 311 Hazardous Categorization: Acute Chronic Fire Pressure Reactive	N/A <u>X</u>	
Section 313 Toxic Chemical Chemical Name CAS N	lumber Conce	entration
CERCLA 102(a)/DOT Hazardous Substances: (+ indicate Seq Chemical Name	s DOT Hazardous CAS Number	Substance Range in 3
None CERCLA/DOT Hazardous Substances (Sequence Numbers a Seq. RQ None		
TSCA Inventory Status: This product, or its components, are listed on or Toxic Substance Control Act (TSCA) Chemical Substa	are exempt fro ince Inventory.	m the
Other: None.		

PRODUCT CODE: 00631



PRODUCT CODE: 00631 NAME: VANGUARD 680 Date Issued: 05-02-96 Supersedes: 12-08-95

14. REGULATORY INFORMATION (CONT)

State Regulations:

California Proposition 65:

The following detectable components of this product are substances, or belong to classes of substances, known to the State of California to cause cancer and/or reproductive toxicity.

Chemical Name CAS Number

None

States Right-to-know Regulations:

Chemical Name State Right-to-know

CALL DIAL OT (CALLED A) EL (FIREME) EL (717/22) MT (MARIA DE LA CALLED A)

State list: CT (Connecticut), FL (Florida), IL (Illinois). MI (Michigan),

LA (Louisiana). MA (Massachusetts), NJ (New Jersey),

PA (Pennsylvania), RI (Rhode Island)

International Regulations:

WHMIS Classification:

Not regulated

Canada Inventory Status:

This product, or its components, are listed on or are exempt from the Canadian Domestic Substance List (DSL).

EINECS Inventory Status:

Not determined.

Australia Inventory Status:

Not determined.

Japan Inventory Status:

Not determined.

15. ENVIRONMENTAL INFORMATION

Aquatic Toxicity:

Not determined.

Mobility:

Not determined

Persistence and Biodegradability:

Not determined.

Potential to Bioaccumulate:

Not evaluated.

Remarks:

Not evaluated.

16. OTHER INFORMATION

None

THE INFORMATION CONTAINED HEREIN IS BELIEVED TO BE ACCURATE. IT IS PROVIDED INDEPENDENTLY OF ANY SALE OF THE PRODUCT FOR PURPOSE OF HAZARD COMMUNICATION AS PART OF TEXACO'S PRODUCT SAFETY PROGRAM. IT IS NOT INTENDED TO CONSTITUTE PERFORMANCE INFORMATION CONCERNING THE PRODUCT. NO EXPRESS WARRANTY, OR IMPLIED WARRANTY OF MERCHANTABILITY OR FITNESS FOR A PARTICULAR PURPOSE IS MADE WITH RESPECT TO THE PRODUCT OR THE INFORMATION CONTAINED HEREIN. DATA SHEETS ARE AVAILABLE FOR ALL TEXACO PRODUCTS. YOU ARE URGED TO OBTAIN DATA SHEETS FOR ALL TEXACO PRODUCTS YOU BUY, PROCESS, USE OR DISTRIBUTE AND YOU ARE ENCOURAGED AND REQUESTED TO ADVISE THOSE WHO MAY COME IN CONTACT WITH SUCH PRODUCTS OF THE INFORMATION CONTAINED HEREIN.

TO DETERMINE APPLICABILITY OR EFFECT OF ANY LAW OR REGULATION WITH RESPECT TO THE PRODUCT, USER SHOULD CONSULT HIS LEGAL ADVISOR OR THE APPROPRIATE GOVERNMENT AGENCY. TEXACO DOES NOT UNDERTAKE TO FURNISH ADVICE ON SUCH

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PRODUCT CODE: 00631 NAME: VANGUARD 680

Date Issued: 05-02-96

Supersedes: 12-08-95



17. PRODUCT LABEL (CONT)

Label Date: 05-02-96

Manufacturer's Name and Address: TEXACO LUBRICANTS COMPANY

A DIVISION OF TEXACO REFINING AND MARKETING INC.

P.O. Box 4427 Houston, TX 77210-4427

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· Message: Here is a	copy of the 10+6
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Diversey Water Technologies Inc

7145 Pine Street P.O. Box 200 Chagrin Falls, OH 44022 Tel: (216) 247-5000 Fax: (216) 247-0745

WATER ANALYSIS REPORT

CUSTOMER #/NAME:

1420000 CANTON SAMPLE #: CANTON DROP FORGING & MFG OH 44706 16810 16811 SALES REP:

FAULK, ROBERT

CITY/STATE/ZIP: ATTENTION:

ROBERT FAULK

DISTRICT:

OHIO VALLEY DISTRICT

SAMPLE INFORMATION 16811 5/07/97 16810 SAMPLE #: 5/07/97 SAMPLE DATE: 5/09/97 5/09/97 LOG-IN DATE: 5/12/97 5/12/97 REPORT DATE: 04:30 PK SAMPLE TIME: 04:30 PM PRODUCTS USED: N/A HPS HPS & FILTERED SAMPLE FROM: 16811 RESULTS 16810 RESULTS PARAMETERS 1 Dil & Grease (SM 5520B) mg/L **APPROVED** REVIEWED BY

THIS ANALYSIS HAS A VALUE OF

\$30.00

\$30.00

Ohio EPA Certificate #1291 for inorganics & #849 for total coliform

* Prepared by Diversey Water Technologies Inc.

CDF002383



Quanterra Incorporated 4101 Shuffel Drive, NW North Canton, Ohio 44720

330 497-9396 Telephone 330 497-0772 Fax



ANALYTICAL REPORT

CANTON DROP FORGE WASTEWATER

Lot #: A7R140153

Michael R. Leffler

Parsons Engineering Science, Inc.

QUANTERRA INCORPORATED

Repecca L. Strait Project Manager

May 29, 1997

EXECUTIVE SUMMARY - Detection Highlights

A7E140153

-		PARAMETER	RESULT	REPORTING LIMIT	UNITS	ANALYTICAL METHOD
	01 CO	IDENSATE TANK 05/13/97 13:30 00	01		:	
		Oil and Grease (Gravimetric)	258	5.0	mg/L	MCAWW 413.1
	02 POI	ND 3 INFL 05/13/97 14:45 002				
25 E	O CE	Oil and Grease (Gravimetric)	8.3	5.0	mg/L	MCAWW 413.1
50 TO	03 HP	S SEPARATOR 05/13/97 14:15 003			. •	
		Oil and Grease (Gravimetric)	1220	5.0	mg/L	MCAWW 413.1
	04 BO	ILER FEED WATER 05/13/97 13:40	004		•	
		Oil and Grease (Gravimetric)	5.4	5.0	mg/L	MCAWW 413.1
	на н	PS BLOWDOWN 05/13/97 14:00 005				
		Calcium Magnesium Hardness, as CaCO3	165 16.8 480	5.0 5.0 4	mg/L mg/L	MCAWW 200.7 MCAWW 200.7 MCAWW 130.2
٠	нав н	PS BLOWDOWN 05/13/97 14:00 006	i		-	
		pH (liquid) Total Dissolved Solids	10.0 310	10	No Units mg/L	MCAWW 150.1 MCAWW 160.1
		Total Alkalinity	2090	25.0	mg/L	SM18 2320 B
	наа в	OILER FEED WATER 05/13/97 13:50	007			•
		Hardness, as CaCO3	8	2	mg/L	MCAWW 130.2
	H2B B	OILER FEED WATER 05/13/97 13:50	008			
		pH (liquid) Total Dissolved Solids	9.7 160	10	No Units	MCAWW 150.1 MCAWW 160.1
		Total Alkalinity	55.2	5.0	mg/L	SM18 2320 B

CASE NARRATIVE

The following report contains the analytical results for eight water samples submitted to Quanterra-North Canton by Parsons Engineering Science, Inc. from the Canton Drop Forge Wastewater Site. The samples were received May 14, 1997, according to documented sample acceptance procedures.

Quanterra utilizes only USEPA approved methods in all analytical work. The samples presented in this report were analyzed for the parameters listed on the following page in accordance with the methods indicated.

The results included in this report have been reviewed for compliance with the laboratory QA/QC plan. All data have been found to be compliant with laboratory protocol.

Supplemental QC Information

GENERAL CHEMISTRY

Matrix spike/matrix spike duplicate spike recovery was outside the acceptance limits for total alkalinity on QC batch 7140229. However, the acceptable LCS analysis data indicated that the analytical system was operating within control and this condition is most likely due to matrix interference.

There are samples reported with dilutions due to either high target analytes or matrix interference.

ANALYTICAL METHODS SUMMARY

A7E140153

PARAMETI	SR	ANALYTICAL METHOD
pH (Elec	ctrometric)	MCAWW 150.1
-	ity. Total	SM18 2320 B
Filteral	ble Residue (TDS)	MCAWW 160.1
Inducti	vely Coupled Plasma (ICP) Metals	MCAWW 200.7
Oil & G	rease (Gravimetric)	MCAWW 413.1
Total H	ardness (Titrimetric, EDTA)	MCAWW 130.2
Referen	ces:	
MCAWW	"Methods for Chemical Analysis of W EPA-600/4-79-020, March 1983 and su	·

"Standard Methods for the Examination of Water and

Wastewater", 18th Edition, 1992.

SM18

SAMPLE SUMMARY

A7E140153

₩O #	SAMPLE#	CLIENT SAMPLE ID	DATE	TIME_
С9КН9	001	01 CONDENSATE TANK	05/13/97	13:30
C9KHD	002	02 POND 3 INFL	05/13/97	14:45
C9KHE	003	03 HPS SEPARATOR	05/13/97	14:15
C9KHF	004	04 BOILER FEED WATER	05/13/97	13:40
C9 KHG	005	H1A HPS BLOWDOWN	05/13/97	14:00
C9KHK	006	H1B HPS BLOWDOWN	05/13/97	14:00
C9KHL	007	H2A BOILER FEED WATER	05/13/97	13:50
C9KHM	008	H2B BOILER FEED WATER	05/13/97	13:50

NOTE (S) :

- The analytical results of the samples listed above are presented on the following pages.
- All calculations are performed before rounding to avoid round-off errors in calculated results.
- Results noted as "ND" were not detected at or above the stated limit.
- This report must not be reproduced, except in full, without the written approval of the laboratory.
- Results for the following parameters are never reported on a dry weight basis: color, corrosivity, density, flashpoint, ignitability, layers, odor, paint filter test, pH, porosity pressure, reactivity, redox potential, specific gravity, spot tests, solids, solubility, temperature, viscosity, and weight.

Client Sample ID: 01 CONDENSATE TANK

General Chemistry

Lot-Sample #...: A7E140153-001 Work Order #...: C9KH9

Matrix....: WATER

Date Sampled...: 05/13/97 13:30 Date Received..: 05/14/97

PREPARATION-

PARAMETER

METHOD

ANALYSIS DATE BATCH #

Oil and Grease

258

mg/L

MCAWW 413.1

05/22/97

7147187

(Gravimetric)

Dilution Factor: 1

Client Sample ID: 02 POND 3 INFL

General Chemistry

Lot-Sample #...: A7E140153-002 Work Order #...: C9KHD

Matrix..... WATER

Date Sampled...: 05/13/97 14:45 Date Received..: 05/14/97

PREPARATION-

PREP

PARAMETER Oil and Grease

8.3

UNITS ng/L

METHOD MCAWW 413.1 ANALYSIS DATE BATCH # 05/22/97

(Gravimetric)

Dilution Factor: 1

RL 5.0

Client Sample ID: 03 HPS SEPARATOR

General Chemistry

Lot-Sample #...: A7E140153-003 Work Order #...: C9KHE Matrix.....: WATER

Date Sampled...: 05/13/97 14:15 Date Received..: 05/14/97

PREPARATION- PREP
PARAMETER RESULT RL UNITS METHOD ANALYSIS DATE BATCH #

Oil and Grease 1220 5.0 mg/L MCAWW 413.1 05/22/97 7147187

(Gravimetric)

Dilution Factor: 1

Client Sample ID: 04 BOILER FEED WATER

General Chemistry

Lot-Sample #...: A7E140153-004 Work Order #...: C9KHF Matrix.....: WATER

Date Sampled...: 05/13/97 13:40 Date Received..: 05/14/97

 PARAMETER
 RESULT
 RL
 UNITS
 METHOD
 ANALYSIS DATE
 BATCH #

 Oil and Grease
 5.4
 5.0
 mg/L
 MCAWW 413.1
 05/22/97
 7147187

(Gravimetric)

Dilution Factor: 1

Client Sample ID: HIA HPS BLOWDOWN

TOTAL Metals

Lot-Sample #...: A7E140153-005 Matrix.....: WATER

Date Sampled...: 05/13/97 14:00 Date Received..: 05/14/97

PREPARATION- WORK

PARAMETER RESULT LIMIT UNITS METHOD ANALYSIS DATE ORDER #

Prep Batch #...: 7135127

Calcium 165 5.0 mg/L MCAWW 200.7 05/15-05/16/97 C9KHG102

Dilution Factor: 1

MCAWW 200.7

mg/L

5.0Dilution Factor: 1

Magnesium

16.8

05/15-05/16/97 C9KHG103

Client Sample ID: HIA HPS BLOWDOWN

General Chemistry

Lot-Sample #...: A7E140153-005

Work Order #...: C9KHG

Matrix..... WATER

Date Sampled...: 05/13/97 14:00 Date Received..: 05/14/97

PREPARATION-

PREP

PARAMETER

RESULT

UNITS

METHOD

ANALYSIS DATE BATCH #

Hardness,

480

mg/L

MCAWW 130.2

05/27/97

7147243

as CaCO3

Dilution Factor: 2

RL

Client Sample ID: H1B HPS BLOWDOWN

General Chemistry

Lot-Sample #...: A7E140153-006 Work Order #...: C9KHK Matrix.....: WATES

Date Sampled...: 05/13/97 14:00 Date Received..: 05/14/97

PARAMETER	RESULT	<u>RL</u>	UNITS	METHOD	PREPARATION- ANALYSIS DATE	PREP BATCH #
pH (liquid)	10.0 Dilution	Factor: 1	No Units	MCAWW 150.1	05/14/97	7134257
Total Alkalinity	2090 Dilution	25.0 Factor: 5	mg/L	SM18 2320 B	05/20/97	7140229
Total Dissolved Solids	310	10	mg/L	MCAWW 160.1	05/19/97	7140268

Dilution Factor: 1

Client Sample ID: H2A BOILER FEED WATER

TOTAL Metals

Lot-Sample #...: A7E140153-007 Matrix....: WATER

Date Sampled...: 05/13/97 13:50 Date Received..: 05/14/97

PARAMETER	RESULT	REPORTING LIMIT	UNITS	METHOD	PREPARATION- ANALYSIS DATE	WORK ORDER #
Prep Batch # Calcium	ND	5.0 ion Factor: 1	mg/L	MCAWW 200.7	05/15-05/16/97	C9KHL102
Magnesium	ND nilu	5.0	mg/L	MCAWW 200.7	05/15-05/16/97	C9KHL103

Client Sample ID: H2A BOILER FEED WATER

General Chemistry

Lot-Sample #...: A7E140153-007 Work Order #...: C9KHL Matrix.....: WATER

Date Sampled...: 05/13/97 13:50 Date Received..: 05/14/97

PREPARATION- PREP
PARAMETER RESULT RL UNITS METHOD ANALYSIS DATE BATCH #

Hardness, 8 2 mg/L MCAWW 130.2 05/27/97 7147243
as CaCO3

Dilution Factor: 1

Client Sample ID: H2B BOILER FEED WATER

General Chemistry

Lot-Sample #...: A7E140153-008 Work Order #...: C9KHM Matrix.....: WATER

Date Sampled...: 05/13/97 13:50 Date Received..: 05/14/97

PARAMETER	RESULT	RL	UNITS	METHOD	PREPARATION- ANALYSIS DATE	PREP BATCH #
pH (liquid)	9.7 Dilution	Factor: 1	No Units	MCAWW 150.1	05/14/97	7134257
Total Alkalinity	55.2 Dilution	5.0 Factor: 1	mg/L	SM18 2320 B	05/20/97	7140229
Total Dissolved Solids	160	10	mg/L	MCAWW 160.1	05/19/97	7140268
	Dilution	Factor: 1				

QUALITY CONTROL SECTION

LABORATORY CONTROL SAMPLE EVALUATION REPORT

TOTAL Metals

Client Lot #...: A7E140153

Matrix..... WATER

PERCENT

RECOVERY

PREPARATION-

Magnesium

RECOVERY

LIMITS

METHOD

ANALYSIS DATE WORK ORDER #

LCS Lot-Sample#: A7E150000-127 Prep Batch #...: 7135127

(80 - 120) MCAWW 200.7

05/15-05/16/97 C9KP212A

Dilution Factor: 1

Calcium

92

97

(80 - 120) MCAWW 200.7 05/15-05/16/97 C9KP2129

Dilution Factor: 1

NOTE (S) :

Calculations are performed before rounding to avoid round-off errors in calculated results.

LABORATORY CONTROL SAMPLE EVALUATION REPORT

General Chemistry

Lot-Sample #...: A7E140153

Matrix: WATER

PARAMETER Oil and Grea (Gravimetr		RECOVERY LIMITS RPD WO#:C9RG8102	RPD LIMITS 2-LCS/C9F	METHOD RG8103-LCSD I	PREPARATION- ANALYSIS DATE LCS Lot-Sample#: A7E2	PREP BATCH # 70000-187
(Gravinetr	108 108	(75 - 125) (75 - 125) 0.46		MCAWW 413.1 MCAWW 413.1	05/22/97 05/22/97	7147187 7147187

NOTE (S):

LABORATORY CONTROL SAMPLE EVALUATION REPORT

General Chemistry

Client Lot #...: A7E140153

Matrix..... WATER

PARAMETER Hardness, as CaCO3	PERCENT RECOVERY		METHOD #: C9RLG102 LCS Lot	PREPARATION- ANALYSIS DATE t-Sample#: A7E270000	PREP BATCH # -243
ab cacos	101	(80 - 120) Dilution Factor: 1	MCAWW 130.2	05/27/97	7147243
Oil and Grease (Gravimetric)		Work Order	#: C9RG8102 LCS Lo	t-Sample#: A7E270000	-187
,,	108	(75 - 125) Dilution Factor: 1	MCAWW 413.1	05/22/97	7147187
Total Alkalinit	Y 110		#: C9ND9102 LCS Lo SM18 2320 B	t-Sample#: A7E200000 05/20/97	-229 7140229
Total Dissolved	l .	Work Order	#: C9NH5102 LCS Lo	t-Sample#: A7E200000	-268
	82	(80 - 120) Dilution Factor: 1	MCAWW 160.1	05/19/97	7140268

NOTE (S):

METHOD BLANK REPORT

TOTAL Metals

Client Lot #...: A7E140153

Matrix WATER

PARAMETER	RESULT	REPORTING LIMIT	G UNITS	METHOD	PREPARATION- ANALYSIS DATE	WORK ORDER #
MB Lot-Sample	#: A7E150	000-127 Prep B	atch #	: 7135127		
Calcium	ND	5.0	mg/L	MCAWW 200.7	05/15-05/16/97	C9KP211L
		Dilution Factor: 1				
Magnesium	ND	5.0	mg/L	MCAWW 200.7	05/15-05/16/97	C9KP211M
		Dilution Factor: 1	-			-
			•			
NOTE (S):		·	<u> </u>			

METHOD BLANK REPORT

General Chemistry

Client Lot #...: A7E140153

Matrix....: WATER

PARAMETER Hardness, as CaCO3	RESULT ND	REPORTING LIMIT Work Order 2 lution Factor: 1	UNITS #: C9RLG101 mg/L	METHOD MB Lot-Sample #: MCAWW 130.2	PREPARATION- ANALYSIS DATE A7E270000-243 05/27/97	PREP BATCH # 7147243
Oil and Grease (Gravimetric)	ND		#: C9RG8101	MB Lot-Sample #:	A7E270000-187	7147187
Total Alkalinity	ND		#: C9ND9101 mg/L	MB Lot-Sample #: SM18 2320 B	A7E200000-229 05/20/97	7140229
Total Dissolved Solids	ND D	Work Order 10 ilution Factor: 1	#: C9NH5101	MB Lot-Sample #:	A7E200000-268	7140268

NOTE (S):

MATRIX SPIKE SAMPLE EVALUATION REPORT

TOTAL Metals

Client Lot # Date Sampled		0153 /97 16:00 Date I	Matrix: WATER .: 05/08/97					
PARAMETER	PERCENT RECOVERY	RECOVERY LIMITS RPD	RPD LIMITS	METHOD	PREPARATION- ANALYSIS DATE	WORK ORDER #		
MS Lot-Samp]	Le #: A7E08	30127-001 Prep 1	Batch #	.: 7135127	•			
Calcium	93	(80 - 120)		MCAWW 200.7	05/15-05/16/97	C9G3813J		
	85	(80 - 120) 7.1	(0-20)	MCAWW 200.7	05/15-05/16/97	C9G3813K		
		Dilution Factor:	1					
Magnesium	96	(80 - 120)		MCAWW 200.7	05/15-05/16/97	C9G3813M		
	89	(80 - 120) 7.1	(0-20)	MCAWW 200.7	05/15-05/16/97	C9G3813N		
		Dilution Factor:	1					

Calculations are performed before rounding to avoid round-off errors in calculated results.

NOTE (S):

MATRIX SPIKE SAMPLE EVALUATION REPORT

General Chemistry

Client Lot #...: A7E140153 Matrix....: WATER

Date Sampled...: 05/13/97 11:25 Date Received..: 05/15/97

PARAMETER	PERCENT RECOVERY	RECOVERY LIMITS	RPD LIMITS METHOD	PREPARATION- PREP ANALYSIS DATE BATCH #
Hardness, as CaCO3		WO#:	C9KHL104-MS/C9KHL105-MSD	MS Lot-Sample #: A7E140153-007
	99	(80 - 120)	MCAWW 130.2	05/27/97 7147243
	99	(80 - 120)	0.0 (0-20) MCAWW 130.2	05/27/97 7147243
		Dilution F	actor: 1	
Total Alkali	nity	WO#:	C9JXW117-MS/C9JXW118-MSD	MS Lot-Sample #: A7E140101-001
	34 N	(80 - 120)	SM18 2320 B	05/20/97 7140229
	34 N	(80 - 120)	0.42 (0-20) SM18 2320 B	05/20/97 7140229
		Dilution F	actor: 1	

NOTE(S):

Calculations are performed before rounding to avoid round-off errors in calculated results.

N Spiked analyte recovery is outside stated control limits.

General Chemistry

Client Lot #...: A7E140153 Work Order #...: C9KLG-SMP Matrix.....: WATER

C9KLG-DUP

Date Sampled...: 05/13/97 12:55 Date Received..: 05/14/97

	DUPLICATE			RPD		PREPARATION-	PREP
PARAM RESULT	RESULT	<u>UNITS</u>	RPD	LIMIT	METHOD	ANALYSIS DATE	BATCH #
pH (liquid)					SD Lot-Sample #:	A7E140166-001	
7.4	7.4	No Units	0.13	(0-20)	MCAWW 150.1	05/14/97	7134257

General Chemistry

Client Lot #...: A7E140153 Work Order #...: C9KLK-SMP Matrix.....: WATER

C9KLK-DUP

Date Sampled...: 05/13/97 14:10 Date Received..: 05/14/97

DUPLICATE PREPARATION-PREP RPD ANALYSIS DATE BATCH # PARAM RESULT RESULT _ LIMIT UNITS RPD METHOD SD Lot-Sample #: A7E140166-002 pH (liquid) 7.3 7.3 No Units 0.14 (0-20) MCAWW 150.1 05/14/97 7134257

General Chemistry

Client Lot #...: A7E140153

Work Order #...: C9KLG-SMP

Matrix....: WATER

C9KLG-DUP

Date Sampled...: 05/13/97 12:55 Date Received..: 05/14/97

DUPLICATE RPD PREPARATION-PREP PARAM RESULT RESULT_ LIMIT ANALYSIS DATE BATCH # UNITS pH (liquid) SD Lot-Sample #: A7E140166-001 7.4 7.4 No Units 0.13 (0-20) MCAWW 150.1 05/14/97 7134257

General Chemistry

Client Lot #...: A7E140153 W

Work Order #...: C9KLK-SMP

Matrix....: WATER

C9KLK-DUP

Date Sampled...: 05/13/97 14:10 Date Received..: 05/14/97

	DUPLICATE			RPD		PREPARATION-	PREP
PARAM RESULT	RESULT	UNITS	RPD	LIMIT	METHOD	ANALYSIS DATE	BATCH #
pH (liquid)					SD Lot-Sample #:	A7E140166-002	
7.3	7.3	No Units	0.14	(0-20)	MCAWW 150.1	05/14/97	7134257
	5. 1						

General Chemistry

Client Lot #...: A7E140153 Work Order #...: C9K0D-SMP Matrix.....: WATER

C9K0D-DUP

Date Sampled...: 05/13/97 12:50 Date Received..: 05/13/97

PARAM RESULT Total Dissolved	DUPLICATE RESULT	UNITS	RPD	RPD LIMIT	METHOD SD Lot-Sample #:	PREPARATION- ANALYSIS DATE A7E140101-003	PREP BATCH #
Solids 1400	1400	mg/L	1.9	(0-20)	MCAWW 160.1	05/19/97	7140268

General Chemistry

Client Lot #...: A7E140153 Work Order #...: C9L0F-SMP Matrix..... WATER

C9L0F-DUP

Date Sampled...: 05/13/97 11:25 Date Received..: 05/15/97

DUPLICATE RPD PREPARATION-PREP LIMIT ANALYSIS DATE BATCH # PARAM RESULT RESULT UNITS RPD METHOD Total Dissolved SD Lot-Sample #: A7E140166-003 Solids 280 280 (0-20) MCAWW 160.1 05/19/97 7140268 mg/L 2.5

General Chemistry

Client Lot #...: A7E140153

Work Order #...: C9F7R-SMP

Matrix....: WATER

C9F7R-DUP

Date Sampled...: 05/01/97 08:15 Date Received..: 05/07/97

<u>PARAM</u> <u>RESULT</u> Hardness,	DUPLICATE RESULT	UNITS	RPD	RPD LIMIT	METHOD SD Lot-Sample #:	PREPARATION- ANALYSIS DATE A7E070109-001	PREP BATCH #
as CaCO3 ND	ND	mg/L	0	(0-20)	MCAWW 130.2	05/27/97	7147243

Chain of Custody Record



QUA-4124-A	····				·			<u> </u>								<u> </u>
Parsons Engineering Scient Address 19101 Villeyicu Road City Cleveland OH Project Name	nee		Project Manager	Plich	ael R L	EF,	FLER	Date 5	1/13	3/9	7	C	hain Ol	Custoo 2 8	885	8
Address July Village Road			Telephone Num	ber (Area Code)/Fax Number	6	1466-6119	Lab Number			-	Т		1		
City State	Zip Code		Site Contact	100 /		216/	486-6117		1.			P	age	alysis	of_	 _
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Contract/Purchase Order/Quote No.		_					~				표	THE	*	agresium		
Sample I.D. No. and Description	Date	Time	Sample Type	Total Volume	Containe Type	ers No.	Preservative	Condition on Receipt	O, (& Grang	Calcium	Total Hardness	Alkalinity	77 d 77 d	MA		
01 CONDENSATE TANK 02 FOR 3 INFL	5/13/97	1:30 PM		10	Glass	1	112504		X						<u> </u>	<u> </u>
03 HPS Separator	5/13/97	2:45pu 2:15p	Water Water	12	Gless	1	H1 SOA		X		4			 -	+-1	
04 R. ler Red Wicker	5/13/97	1:40pm	Water	12	در لوچې	1	H2504 H2504		X	\dashv	\dashv	\dashv	-		+-+	++-
					<u> </u>	-4-	1/2 - 4	1	Α .	-+	+	-				+
HIA HPS Blowdown	5/13/97	2:00,14		500m	B	1	HNO3	<u> </u>		X				X		
HIB HPS Blowdown	5/13/97	2 20 pm	unter	500ml	, <u>, , , , , , , , , , , , , , , , , , </u>	1	NOTES HA			-	}	Χχ	X		+	
H2A Biler Feed Water	5/13/97	1:50pm	water-	50041	500mlP	7	1+103			X	\times		+	X	+	+
428 Boiler Feed Water	5/13/97	1:52pm	water	500in (P	i	NONE			7	<u> </u>	XX	(X		 	+++-
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ELE lludson Industries

Box 2212 • Hudson, Ohio 44236-0812 • 216-487-0668 • FAX 216-487-0811

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BILL TO

FORM COF 41 5M

Canton Drop Forge 4575 Southway Street, S.W. Canton, OH 44706 SHIP TO

Canton Drop Forge 4575 Southway Street, S.W. Canton, OH 44706

Attn: Stockroom

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CLEVELAND TECHNICAL CENTER



18419 EUCLID AVENUE, CLEVELAND, OHIO 44112-1016 (800) 726-5400, FAX (216) 383-9633

DESCRIPTION: CYLINDER OIL

CUSTOMER NO.: 10605

UNIT NO.: 2-CDF

MAKE:

MODEL:

OIL BRAND: OIL TYPE:

UNIT SERIAL NO:

FUEL TYPE:

NO. COPIES: 1

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CANTON DROP FORGE
BOX 6902 4575 SOUTHWAY ST S W
CANTON, OH 44706



CLEVELAND TECHNICAL CENTER



18419 EUCLID AVENUE, CLEVELAND, OHIO 44112-1016 (800) 726-5400, FAX (216) 383-9633

UNIT SERIAL NO:.

DESCRIPTION: CYLINDER OIL

CUSTOMER NO.: 10605

UNIT NO.: 1-CDF

MAKE:

MODEL:

OIL BRAND: OIL TYPE:

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CANTON DROP FORGE BOX 6902 4575 SOUTHWAY ST S W CANTON, OH 44706

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CLEVELAND TECHNICAL CENTER



18419 EUCLID AVENUE, CLEVELAND, OHIO 44112-1016 (800) 726-5400, FAX (216) 383-9633

DESCRIPTION: CYLINDER OIL

CUSTOMER NO.: 10605

UNIT NO.: 3-CDF

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CANTON DROP FORGE
BOX 6902 4575 SOUTHWAY ST S W
CANTON, OH 44706

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May 27, 1997

I/ - MOBN EXTRA HECLA

#2 - CITGO 680-7 #3-TEXACO VANGUARD 680

Bob ROBIE 1-800-726-5400

ASTM Demulsibility Testing

Canton Drop Forge ATTN: Mr. Keith Houseknecht Manager, Plant Engineering 4575 Southway Street S.W. Canton, OH 44706

Dear Keith,

Please find enclosed a pint sample of Mobil Extra Hecla Super Cylinder Oil for your use in testing its demulsibility rating vs. the competitive product now in use.

I contacted the lab manager at Cleveland Technical Center to find out for you whether or not the laboratory could run the ASTM Demulsibility Procedure. They are able to complete this test, charging approximately \$52.50 per sample. You should allow a couple of weeks for the results to be completed and returned to you.

You can mail the samples to:

Cleveland Technical Center 18419 Euclid Avenue Cleveland, OH 44112-1016

Phone: 1-800-726-5400

PRESSURE COPY EX

When you have the results, Keith, I would appreciate any feedback you can give me regarding the results. Should you need any further assistance in this matter, or if there are other areas where we can be of assistance, please give me a call at 1-800-392-7834, voice mail extension 312.

I will continue to monitor Mobil's development of the new synthetic product we discussed and update you when the information is available.

Respectfully submitted;

Neil F. Hasson

Senior Lubrication Engineer

Ken Ullman

Integrity - Value - Service

CDF002419

CLEVELAND IECHNICAL CENTER



JUN-13-97 FRI 11:51

CLEVELAND TECHNICAL CTR.

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18419 EUCLID AVENUE, CLEVELAND, DN10 44112-1016 (800) 726-5400, FAX (216) 383-9633 DESCRIPTION; CYLINDER DIL

CUSTOMER NO.: 10605

CANTON DROP FORGE

PHONE # (999) 999-9999 FAX # (000) 000-0000

UNIT NO.: 1-CDF

MAKE:

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DIL TYPE:

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18419 EUCLID AVENUE, CLEVELAND, OHIO 44112-1016 (800) 726-5400, FAX (216) 383-9633

DESCRIPTION: CYLINDER OIL

CUSTOMER NO.: 10605

UNIT NO.: 3-CDF

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UNIT SERIAL NO:.

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CANTON DROP FORGE PHONE # (999) 999-9999 FAX # (000) 000-0000

WHEN CORRECTIVE ACTION IS INDICATED, PLEASE ADVISE RESULTS OF YOUR FINDINGS AND CORRECTIVE ACTION TAKEN ON ENCLOSED FORM.

Since Spectra-Check services are based on samples and information supplied by others, and since corrective action, if any, is necessarily taken by others, these services are rendered without any warranty or hability of any kind

CLEVELAND IECHNICAL CENTER



18419 EUCLID AVENUE, CLEVELAND, ONIO 44112-1016 (800) 726-5400, FAX (216) 383-9633

DESCRIPTION: CYLINDER OIL

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CLEVELAND TECHNICAL CTR.

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Fax# 330-477-2046	Fax#

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CANTON DROP FORGE PROCESS WATER AND WASTEWATER RECYCLING/TREATMENT INVESTIGATION SUMMARY REPORT

TO 5024

Introduction

Canton Drop Forge generates a number of process water and wastewater streams, primarily derived from boiler water treatment, condensate and cooling water streams. Some of the wastewater is discharged to the sanitary sewer system for treatment at the City of Massillon wastewater treatment plant; the remaining streams are discharged to an on-site pond system which also handles the site storm water drainage. Wastewater streams are discharged to Pond 2, which is equipped with an oil skimmer and which removes floating oils which may reach the pond. The discharge of Pond 2 is pumped to Pond 3. There is no surface discharge from Pond 3.

All water at the facility comes from Canton Drop Forge wells. Water production is not recorded.

The purposes of this investigation are to identify the most appropriate alternatives for treating, recycling, and/or disposing of the process water and wastewater streams generated by Canton Drop Forge and to avoid discharge of oil-contaminated streams to the on-site ponds. Of primary interest is the condensate flow which contains solubilized oils that do not separate readily in a gravity oil/water separator.

Process Water and Wastewater Streams

Condensate

High pressure steam (150 psig) is generated by two gas boilers and one coal-fired boiler for plant use. Well water is treated by a hot process softener (HPS) and filtered through anthracite filters prior to being fed to the boilers. The high pressure steam is primarily used to lift the hammers at the drop forges, but some may be used for building heat. Before entering the hammer lift cylinders, oil (Citgo Cylinder Oil 680-7) is injected into the steam. The exhaust from the cylinders is captured in the low pressure steam header (6 to 8 psig) and distributed for other uses. The low pressure steam (which has been injected with cylinder oil) is used to heat the HPS (direct steam injection), for anvil heating, and for building heat throughout the facilities. Excess low pressure

steam is exhausted to atmosphere through a baffled separator and multi-port valve to maintain header pressure. The vented flow is measured and has been recorded over recent months. Visual examination of the data indicates that the average venting rate is approximately 12 to 15 million cubic feet per day during drop forge operation.

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Condensate from the various area heaters, located throughout the facility, generally flows to the nearest drain and then ultimately to Pond 2. Because of the scattered locations of these heaters, no consideration was given in this study to collecting these streams.

The major sources of oil-contaminated condensate are the baffled separator on the low pressure steam exhaust, the separator on the steam line to the HPS, and the anvil heating lines. These flows have recently been routed to a 1500-gallon horizontal tank from which they drain to Pond 2. Water is drained from near the bottom of the tank through an elevated pipe which can be adjusted to maintain the water level in the tank at approximately 6 to 15 inches.

Mr. Keith Houseknecht, Manager of Plant Engineering for Canton Drop Forge, has estimated the total condensate flow at 3 gpm.

Die lube/condensate

Mineral oil with graphite (DUBRO 500/550) is used on the forge dies and Ebery by to be supply is drained with any condensate collected in the area to a gravity oil/water separator. The separated oil is returned to DUBRO Oil Corporation for reconditioning and returned for reuse. The underflow water is discharged to Pond 2.

No estimate of the flow from this stream is available.

Cooling Water (Recirculating System) Overflow

A recirculating cooling water system is provides cooling water and seal water to the furnaces and cooling water to the hydraulic presses.) After use, the cooling water is collected in a cooling water return sump and returned through a cooling tower to the supply sump. The internals of the cooling tower have been dismantled and removed; now the return stream simply discharges at the top of the tower and free falls to the supply sump. Make-up well water is added to the supply sump based on the level. An overflow pipe from the supply sump discharges to Pond 2.

No estimate of the make-up water requirements is available.

Plant air is provided by an Ingersoil-Rand, water-cooled air compressor. Well water is used in the compressor oil cooler and after-cooler, then discharged to the circulating system supply sump. During the period that Parsons ES

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observed the system operation on 13 May 1997, it appeared that the compressor cooling water supply exceeded the need for make-up water in the recirculating system, as the overflow operated, every time that the return pumps ran. - BONTINGUSEY, EVENS WHEN THE

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Coal-fired Boiler Scrubber Discharge

RECIEL, WATER The coal-fired boiler exhaust is equipped with a scrubber. Four to five gallons per minute (gpm) of well water are sprayed into the top of the tower, 4 while the bulk of the scrubber water is recirculated and treated with lime and polymer. Sludge from the recirculated water tank is pumped to a hopper and excess water overflows to Pond 2. Overflow from the recirculation tank, as well as condensate from the boiler exhaust fan, also flows to Pond 2. The coal-fired boiler (and thus the scrubber system) is not regularly used, but is used periodically every winter. Facility records for January through April 1997 indicate that the coal-fired boiler was used for six days in January and 14 days in March.

Allowing for evaporation, the discharge should be less than the 4 to 5 gallons per minute of well water sprayed into the top of the scrubber.

HPS Blowdown

Chemical precipitates formed in the HPS are discharged to the sanitary sewer system . A 3/4" line runs continuously to limit solids build-up and a larger by line (two or three inch) is manually opened one or two times a shift for a short period to remove larger solids that accumulate in the bottom of the tank. It is reported that lime solids from the process have collected in the sanitary sewer system for distances as great as one mile from the discharge point.

No estimate of the flow rate is available.

Boiler Blowdown

Continuous surface blowdown from the boilers and periodic blowdown of the mud drums is also discharged to the sanitary sewers.

No estimate of the flow rate is available.

Potential Use/Disposal of Process Water and Wastewater Streams

HPS Make-up Water

All boiler feed water is treated in the HPS. Most of the water is sourced from the on-site production wells; the only exception is the amount which results from the condensation of the low pressure steam that is injected into the unit for heating. A simple heat balance (neglecting heat losses through the tank walls and blowdown) indicates that approximately 173,500 gallons of well water and 253,500 pounds of low pressure steam are required per day to generate 1.7

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million pounds of high pressure steam per day (the average production during system operation in April 1997). The condensed steam contributes 30,500 gallons to the boiler feed water stream.

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- 〜アC& DAY Coolina Water

Once-through cooling water is used in the plant air compressor and then discharged to the recirculating cooling system. Make-up water can also be added to the recirculating system as required. No measurement of either water flow is available. According to the air compressor manufacturer, total heat rejection from the unit is 607,000 BTU/hr. Recommended cooling water flow rates are based on a maximum exit temperature of 120° F. At an inlet water temperature of 60° F (assumed well water temperature), the recommended flow rate would be 20 gpm. Although the flow rate was not measured, it appears that a higher flow rate is used for air compressor cooling. As stated above, it appears that the compressor cooling water discharge exceeds the make-up requirements of the recirculating system.

Coal-fired Boiler Scrubber Water

The scrubber system uses 4 to 5 gpm of well water when operating. Since the coal-fired boiler only operates periodically, this water use is not always available.

Water Sampling and Analysis

On 13 May 1997, ten (10) samples were collected from six (6) sampling points (see below) and submitted for chemical analysis and for treatability testing. In addition, pH and temperature measurements were made at several of the sampling points at the same time. The laboratory results reported by Quanterra Environmental Services are attached and are summarized, along with the field data (i.e., pH and temperature), in Table 1. Following is a brief description of each sample point.

Of Condensate Tank—The conditions are collected from six (6) sampling points.

O1 Condensate Tank — The sample was collected from a sample valve on the discharge from the 1,500 gallon tank where the three oily condensate streams are combined before discharge to Pond 2.

<u>O2 Pond 3 Influent</u> — The sample was taken from below the surface of the pond in the inlet where the effluent from Pond 2 is discharged into Pond 3.

O3 HPS Separator Discharge — To collect this sample, the discharge from the HPS separator was temporarily routed outside (of the building), through existing piping which previously was used to discharge to Pond 2. The sample represents the discharge from the bottom of the separator and does not include drainage from the steam pipe leading to the separator.

				Table	1 = Trysti	11 12 14 14				
			S	ampling R	esults	1.1.	* :	**		
					<u> </u>	:				·
SAMPLE	DATE	TIME	Temp (C)	O&G	/pH	TDS	Alk.	Ca	Mg	Hard.
Condensate Tank	5/13/97	13:30	80.8	258	9.1					
Pond 3 Inlet	5/13/97	14:45		8.3)					
HPS Separator Blowdown	5/13/97	14:15		1220						
Boiler Feed Water	5/13/97	13:40		5.4						
Boiler Feed Water	5/13/97	13:50			9.7	160	55.2	<5	<5	3
HPS Blowdown	5/13/97	14:00			10	310	2090	165	16.8	480
*pH in S.U., all others in mo	/L; hardnes	s and alka	linity are in	mg/L as C						

MUSS BE UP AROUND 10PM

DUE TO SODA & SUSPENSION OF STAY IN SUSPENSION

<u>O4 Boiler Feed Water</u> — The sample was collected downstream of the anthracite filters, at the same location used by the boiler operators for routine boiler feed water tests.

<u>H1 (A and B) HPS Blowdown</u> — The sample was collected from the large blowdown line (on the bottom of the HPS), which is used by the operator for periodic system blowdown. Two samples were required because of different preservatives required for the analyses to be conducted.

<u>H2 (A and B) Boiler Feed Water</u> — Samples were collected at the same location as O4 above. Two samples were required because of different preservatives required for the analyses to be conducted.

Treatability Testing

Two five-gallon buckets of condensate were also collected from the 1,500-gallon tank (same location as sample O1 above). One bucket was sent to KOCH membrane systems for testing and the other was sent to Parsons ES in Syracuse, New York, for screening of other alternatives.

Membrane Filtration

KOCH Membrane Systems treated a portion of the supplied condensate through a membrane filter. They reported that the sample filtered very well, producing a clear filtrate with an O&G concentration of less than 2 mg/L. Samples of the resulting filtrate and concentrate were sent to you for visual observation. In the treatability testing, KOCH did not run the tests for a period long enough to fully concentrate the retentate. They report that the oil and grease (O&G) can be concentrated to about 25% with their hollow fiber unit and to 50% with their tubular unit. For an inlet O&G concentration of 250 mg/L, this represents a 1,000 or 2,000 fold increase in concentration.

KOCH has submitted proposals for both types (i.e., hollow fiber and tubular) of systems. A binder containing these quotes and other information was prepared for you by KOCH and is enclosed.

Screening Tests

Mr. Douglas Morrison, of Parsons ES' Syracuse Office, conducted a number of qualitative tests to identify other methods to potentially remove the oil from the condensate. These are summarized below:

Gravity Separation

Approximately one-third gallon of the condensate sample was allowed to settle over-right. No oil separation was observed.

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Acid Cracking

Sulfuric acid was added to lower the pH to less than 2.0. No separation was observed in the first three to four hours but, after approximately 15 hours, a separate oil layer was observed.

Caustic

Sodium hydroxide was added to raise the pH above 13.0. The sample was checked after approximately 15 hours, but no oil separation was observed.

High Temperature

The sample was heated to above 90° C while mixing. No oil separation was observed during heating or subsequently cooling to room temperature.

Low Temperature

The temperature was decreased to 4° C. After 24 hours, no oil separation was observed.

Alum Addition

A high dosage of aluminum sulfate (alum) was added. There was no immediate effect but, after about 15 hours, a thin oil layer had formed and oily globules were observed at the bottom of the beaker. The middle layer was very clear.

Sodium Chloride Addition

A high dosage of sodium chloride was added to the sample. There was no immediate effect but, after about 15 hours, a distinct oil layer had formed with clear liquid below.

Filtration

An attempt to filter the sample through a 0.45 micron filter was made but the filter blinded almost immediately. A coarser filter (500 to 1,000 microns), generally used by Canton Drop Forge as a pre-filter, was then used and resulted in a clear filtrate and dark retentate. To verify that the retentate was O&G, the filter was rinsed with hexane. The hexane dissolved all of the visible material on the filter indicating that the retentate was O&G. Hexane was also applied to the filtrate to see if additional oil could be visibly removed. No change in appearance of the filtrate was observed.

Simple Filtration

Because of the apparent success of the filtration screening test, the remainder of the sample sent to Syracuse was delivered to a local laboratory for quantitative filtration testing. Samples were filtered using 500 micron, 25 micron, and 10 micron filters. The filtrate from each test was analyzed for O&G and the solids captured on the filter were measured. The results are presented in Table 2.

Table 2
Filtration Testing Results

		I litteriori i ootii ig i toosii	
·	Filter Size	Filtrate O&G	Solids removed by filter
. و	No Filter	20 mg/L	
was -	500 micron	24 mg/L	<4 mg/L
HOW SOED	25 micron	15 mg/L	5.7 mg/L
NODE 27	10 micron	11 mg/L	9.4 mg/L
BY FILTER		dicate that low effluent O&G	concentrations can be

These results indicate that low effluent O&G concentrations can be achieved through coarse filtration. Unfortunately, the analysis without filtration shows an influent O&G concentration of only 20 mg/L as opposed to the 258 mg/L reported by Quanterra Environmental Services. Although the sample was quite aged by the time that these tests were run, it is not anticipated that such a drastic reduction in the O&G concentration could have occurred. Another possibility is that O&G plated out on the plastic liner in the sample bucket used for transport. Again, it is not anticipated that this could result in such a drastic change in concentration. KOCH has since analyzed their sample for comparison; after three (3) weeks (without any steps taken towards preservation) since collection, the results have indicated that 92.9 mg/L of O&G was still present. Obviously, the results above are not consistent with those provided in the laboratory analyses completed by Quanterra and KOCH. The implication of these findings, as indicated in our recommendations, is that on-site testing with the selected technology should be completed prior to final design

Previously Conducted Tests

and installation.

Information included in annual reports on boiler water treatment, submitted to Canton Drop Forge by Diversey Water Technologies, indicate that the O&G concentration in the condensate can be reduced to 4 to 13 mg/L through treatment by ferric chloride and polymers.

Evaluation of Alternatives

Wastewater Streams

The estimated volume and quality of the process water and wastewater streams, as they are currently generated, are summarized in Table 3. Information is presented for the period when the forges are operating (generally four days per week).

CDFRPT.DOC Page 7 6/6/97 4:46 PM Table 3
Process Water and Wastewater Streams

Stream	Estimated Flow	Characteristics	Notes
Condensate	3 gpm	O&G = 250 mg/L Temperature is ~ 84° C.	Should be rather clean except for oil because it is derived from steam.
Die Lube/ Condensate	Unknown	May contain oil carry-over if O/W Separator is over-loaded. Residual oil concentration unknown	Apparently good oil separation occurs in the O/W Separator.
Recirculating System Overflow	Unknown	No significant oil contamination. May contain contaminants picked up from furnace seals.	
Coal-fired Boiler Scrubber Discharge	< 5 gpm	May contain contaminants from stack gas. Water is treated with lime and polymer before discharge.	
HPS Blowdown	Unknown	pH = 10, TDS = 310, and Temperature is ~ 100° C. Contains calcium carbonate. May be oversaturated with calcium, resulting in scaling properties.	Is currently discharged to the sanitary sewer.
Boiler Blowdown	Unknown	High purity water with some boiler treatment chemicals and inerts. Temperature is ~ 100° C.	Is currently discharged to the sanitary sewer.

Water Uses

The estimated usage and water quality requirements for candidate recycled water users are presented in Table 4. Information is presented for the period when the forges are operating (generally four days per week).

Table 4 Water Uses

Use	Estimated Flow	Required Water Quality	Notes
HPS Feed Water	173,500 gallons per day (120 gpm)	Restricted to contaminants which can be removed in HPS. System can remove some O&G.	High water temperature is acceptable
Air Compressor Cooling Water	20+ gpm	Non-scaling Non-corrosive <100° F	Required flow rate increases with increasing water temperature
Recirculating Cooling Water	Unknown	Non-scaling Non-corrosive <100° F	
Coal-fired Boiler Scrubber Water	4 to 5 gpm	Non-scaling	

Alternatives

Although further investigation may be warranted, there are no known problems with the process water and wastewater streams, except the oily condensate and the reported solids deposition in the sanitary sewer from the HPS blowdown. The focus of this study is elimination of the soluble oil in the condensate discharge to Pond 2.

Alternatives for disposal of the oily condensate (with or without further treatment) fall in three general categories—continued discharge to the pond system, discharge to the sanitary sewer system, and reuse somewhere at the facility. Treatment alternatives depend on the final disposition of the water and the required water quality. Treatment methods identified, which are effective to some degree for removing oil from the condensate, include membrane filtration, conventional filtration, ferric chloride/polymer treatment, acid treatment, alum treatment, and sodium chloride treatment.

Final Disposal

Discharge to Pond System

If the wastewater stream is discharged to the pond system, one or more environmental permits may be required. Since there is no off-site discharge from the pond system, typical discharge limits prophably do not apply to Canton Drop Forge. Although the limit for O&G in a wastewater discharged directly to a receiving stream is normally about 10 mg/L, the limit may be more restrictive in this case. Discussions with Ohio EPA, which have not been undertaken, would be required to verify the water quality requirements for this option.

Discharge to Sanitary Sewer

The City of Massillon sewer use ordinance limits the O&G concentration of any discharge to 100 mg/L. Other limitations which might impact discharge of the condensate are that the pH can not be less than 5.0 or higher than 10 and the temperature "at the introduction into the City's wastewater treatment plant" cannot exceed 40 degrees Celsius (104° F)". No other known pollutants of concern are in the condensate, but the City may require further testing before accepting the discharge.

Reuse

The four potential locations identified for water reuse are summarized in Table 4. Of these, the two cooling water streams do not appear to be very practical because of the high temperature of the condensate. The condensate would have to be cooled considerably before use as a cooling water.

Reuse in the coal-fired boiler scrubber appears to be possible with limited pre-treatment of the condensate. Because of the intermittent nature of the scrubber operation, this disposal alternative is not available the majority of the time and, therefore, does not provide a means for continuous disposal of the condensate.

The only viable reuse alternative appears to be use as feed water to the HPS. This would require a high degree of oil removal but the high condensate temperature would be an advantage rather than a detriment to the process. Use of hot condensate as part of the feed water would reduce the steam requirement to heat the incoming feed water. A simplified heat balance indicates that the steam requirement would be reduced by approximately 6,000 lb/day.

The major concern with reuse of the condensate is the impact of any residual oil on the receiving system. Membrane-filtered condensate with an oil concentration less than 2 mg/L would probably not impact the system. The HPS system may adequately handle higher concentrations. One concern is the measured O&G concentration of 5.4 mg/L in the boiler feed water. This is near the detection limit for the test and, therefore, may be suspect. However, it is

CDFRPT.DOC Page 10 6/6/97 4:46 PM desirable that the O&G concentration in the boiler feed water be less than 1.0 mg/L. Further testing should be conducted to confirm that the O&G concentration is really this high.

If O&G is getting into the boiler feed water, the most likely source is the low pressure steam used to heat the HPS. The discharge from the separator (on the steam line) to the HPS had a high O&G concentration (although the flow rate was very low), indicating that oil is being carried with the steam to at least that point. Theoretically, reducing the steam use by using hot condensate with low O&G content, would reduce the oil contamination from the source. However, the estimated reduction in steam use is only about 2.5 percent. Flocculant systems are available to remove O&G from boiler feed water, if needed.

Treatment Options

Membrane Filtration

The treatability testing using a membrane filter indicated that the O&G concentration of the condensate can be reduced to less than 2 mg/L. KOCH has proposed two different units that can do the job; however, both require a significant reduction in the condensate temperature because of temperature limitations of the membranes. The hollow fiber system would cost \$34,000 and would require the temperature to be reduced to 113° F or less. This unit has a smaller foot print than the tubular system but can only concentrate the retentate to about 25 percent O&G.

The tubular system costs \$41,500 and requires a temperature reduction to at least 140° F. This unit is capable of concentrating the retentate to approximately 50 percent O&G.

KOCH indicates that higher temperature membranes can be supplied, but they will result in a lesser quality filtrate and will increase the cost of the unit by a factor of 1.5 to 2. Parsons ES has requested information from other manufacturers regarding high temperature membranes.

Conventional Filtration

Conventional filtration appears to provide good oil removal. Based on the tests described above, the O&G in the treated condensate may not be low enough for reuse in the HPS or discharge to the pond system, but would easily meet the City's requirements for discharge to the sanitary sewer. This option can be further evaluated by installing a temporary pump and cartridge filter. The system could be run for a few days to determine the life of the filter cartridges and to obtain additional discharge samples to determine the achievable O&G concentration. A permanent system using a high temperature condensate pump and cartridge filters could be installed for less than \$5,000.

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Chemical Treatment

Testing of a number of chemical treatment options has identified which can reduce the O&G concentration to a low level. Canton Drop Forge has indicated that a primary objective of this effort is to implement a system requiring minimal operator attention. Since these alternatives do not fulfill this requirement, they were not evaluated further.

Alternative Oil for Cylinder Lubrication

Canton Drop Forge is investigating alternative oils for injection into the steam supply to the cylinders, which may be less likely to solubilize in the condensate. This appears to be a worthwhile effort, which may result in an oil that is more readily separated from the condensate and/or may result in less carry-over of oil to the HPS.

Recommendations

The best alternatives for disposal of the condensate appear to be treatment through cartridge filters and discharge to the sanitary sewer or treatment through cartridge filters (or membrane filters, if necessary), and reuse in the HPS. Before pursuing either course of action, the following actions are recommended.

- 1. Monitor the condensate stream to determine the average and peak flow rates. The simplest method of flow measurement would be to operate the 1,500 gallon condensate tank in a fill-and-draw method, while monitoring the time required to fill the tank.
- 2. Install a temporary cartridge filtration system (acquired by borrowing or leasing a unit from a prospective supplier) to evaluate the cartridge change frequency and the sustained effluent quality obtainable.
- 3. If results are satisfactory and it is desired to discharge to the sanitary sewer, discuss proposed discharge with the City of Massillon to define requirements for further testing/applications.
- 4. If it is desired to use treated condensate in the HPS, further sampling of the boiler feed water should be conducted to determine the present O&G concentration. Discussions should be held with the HPS manufacturer, the boiler manufacturer, and/or the boiler water treatment specialists to confirm the limitations on the O&G concentration in the HPS feed water.
- 5. If sufficient O&G reduction cannot be obtained by using a cartridge filter, arrange for on-site testing of one or membrane filters to verify the achievable performance and sizing parameters.

ARE

HPS Blowdown

It has been reported that the City of Massillon's sanitary sewer authority is reluctant to accept the condensate flow because of the reported problems with solids deposition from the HPS blowdown. Discharge of lime sludge to sanitary/ sewer systems is not unusual. The sample analysis of this study indicates that the blowdown is over-saturated with calcium but, because of the calcium carbonate solids in the blowdown, any precipitation probably occurs on the solids rather than on the pipe walls. If solids are building up in the sewer, it probably indicates that there is not sufficient flow to maintain the solids in suspension. Several options are available for improving this situation. These are:

- The point of discharge of the blowdown to the sanitary sewer could be 1. relocated to a place where more flow is present on a continuous basis.
- The bloodown could be modified by eliminating the small continuous 2. blowdown and using only the periodic manual blowdown. Ideally a schedule could be established that would maintain the treated water quality while using less frequent blowdown at a higher flow rate to keep the solids flowing in the sewer. The blowdown could be automated to eliminate dependence on manual operation.
- If it is decided to discharge treated condensate to the sanitary sewer, the additional flow may be used to advantage to assist in keeping the solids flowing in the line.

Summary

In summary, Parsons ES recommends that Canton Drop Forge consider use of cartridge filters for treatment of the oil-contaminated condensate stream. Prior to purchasing and installing a cartridge filtration system, it is recommended that certain measurements and observations be made and a trial application be made. If successful in reducing oil content to the desired levels, the resulting John Androws stream can then be discharged to the HPS or the sanitary sewer. This option can be accomplished for \$5,000, or less, provided that the prospective equipment vendor(s) is(are) willing to loan Canton Drop Forge a system for prepurchase treatability testing.

With respect to the HPS blowdown, the recommendations listed above could be implemented. By combining the two streams and, hence, increasing the flow, the HPS blowdown issue may also be resolved.

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29 May 1997

MEMORANDUM

To:

Mr. Keith Houseknecht, Canton Drop Forge

Fax: (330) 477-2045

From:

M. R. Leffler, Parsons ES

Subject:

Wastewater Recycling and/or Treatment

Here is a brief summary of our findings to date. All results and observations should be considered preliminary.

Samples were collected and delivered to Quanterra Environmental
Services for analysis. The results of these analysis with some field pH
and temperature measurements are summarized on the attached table.
The Pond 3 inlet sample was collected from the pond in a small inlet near
the point of discharge from Pond 2.

The oil & grease concentration in the condensate tank was 258 mg/L which is on the low side, but in the range you had previously reported. The HPS separator blowdown was significantly higher. Note that there is 5.4 mg/L of oil & grease in the boiler feed water. This is near the detection limit of 5.0 for the analysis, but indicates that oil and grease is getting through the HPS system.

- 2. A five gallon sample from the condensate tank was sent to KOCH Membrane Systems for trial ultra-filtration. They reported that the material filtered very well producing a clear filtrate with an oil & grease concentration of <2 mg/L. They returned samples to you. KOCH did not run the sample to maximum retentate concentration because of limited sample volume. They say that it could be concentrated to 25 to 30% oil and grease. Starting with 250 mg/L oil & grease in the condensate, the concentration ratio would be 1,000 to 1 or greater. KOCH has not yet provided sizing and cost data.
- 3. I also sent a five gallon sample of the condensate to our Syracuse office for testing. They did qualitative tests for emulsion breaking by trying various methods and visually observing for oil separation. Methods tested were gravity separation, acid cracking, caustic cracking, high temperature (90 °C), low temperature (4 °C), alum addition, sodium chloride addition, and filtration. Except for filtration, no test produced immediately results; however, when allowed to set overnight (15 hours), separation was observed in the samples treated with acid, alum, and sodium chloride. Filtration through a fine filter (0.45 micron) plugged the

filter immediately, but filtration through a coarse filter (500 to 1000 micron) produced a clear filtrate and a dark retentate. Qualitative testing indicated that the retentate was essentially all oil and grease.

4. Since simple filtration looked favorable, our Syracuse office sent the remaining sample out to a local lab for filtration testing. They reported the following results:

Filter Size	Filtrate O&G	Solids removed by filter
No Filter	20 mg/L	
500 micron	24 mg/L	<4 mg/L
25 micron	15 mg/L	5.7 mg/L
10 micron	11 mg/L	9.4 mg/L

The oil & grease analysis with no filtration is an order of magnitude different than the results obtained from Quanterra. We are checking this number. The results indicate that simple filtration reduce the oil & grease to low levels.

5. Preliminary options analysis—Apparently ultrafiltration will clean the condensate to a high level, but simple filtration might be sufficient at much lower cost. We are considering recommending an on site with a cartridge filter to see how frequently filter changes may be required, and what quality of effluent can be obtained.

The best candidate for recycling appears to be to return the condensate to the hot process softener. This process can handle some oil and grease, but since there is already measurable oil and grease in the boiler feed water, it may not be desirable to introduce more oil and grease into the process.

The other continuous water user identified is the compressor cooling water system. This once-through flow discharges to the furnace cooling system. To be used as cooling water, the condensate would have to be cooled. It appears that the cooling water flow exceeds the need for make-up water in the furnace cooling water system so the treated condensate would still be discharged to Pond 2.

The City of Massilon sewer use ordinance limits oil & grease to 100 mg/L; therefore, it would not be difficult to meet this limit through simple filtration. Other limits of concern are maximum pH 10 and maximum temperature of 104 °F at the entrance to the treatment plant.

Because of the high oil and grease in the HPS separator blowdown, and the presence of oil and grease in the boiler feed water, there is apparently significant oil and grease carried over in the steam to the HPS. Your

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SAMPLE	DATE	TIME	Temp (C)	O&G	<u>і</u> /рН		TDS	Alk.	Ca	Mg	Hard.
Condensate Tank	5/13/97	13:30	80.8	258		9.1					
Pond 3 Inlet	5/13/97	14:45		8.3							
HPS Separator Blowdown	5/13/97	14:15		1220		•					
Boiler Feed Water	5/13/97	13:40	· · · · · · · · · · · · · · · · · · ·	5.4						<u> </u>	
Boiler Feed Water	5/13/97	13:50				9.7	160	55.2	<5	<5	- 1
HPS Blowdown	5/13/97	14:00				10	310	2090	165	16.8	480
*pH in S.U., all others in m	ig/L								<u> </u>		

Sheet1

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CANTON DROP FORGE PROCESS WATER AND WASTEWATER RECYCLING/TREATMENT INVESTIGATION SUMMARY REPORT

Introduction

Canton Drop Forge generates a number of process water and wastewater streams, primarily derived from boiler water treatment, condensate and cooling water streams. Some of the wastewater is discharged to the sanitary sewer system for treatment at the City of Massillon wastewater treatment plant; the remaining streams are discharged to an on-site pond system which also handles the site storm water drainage. Wastewater streams are discharged to Pond 2, which is equipped with an oil skimmer and which removes floating oils which may reach the pond. The discharge of Pond 2 is pumped to Pond 3. There is no surface discharge from Pond 3.

All water at the facility comes from Canton Drop Forge wells. Water production is not recorded.

The purposes of this investigation are to identify the most appropriate alternatives for treating, recycling, and/or disposing of the process water and wastewater streams generated by Canton Drop Forge and to avoid discharge of oil-contaminated streams to the on-site ponds. Of primary interest is the condensate flow which contains solubilized oils that do not separate readily in a gravity oil/water separator.

Process Water and Wastewater Streams

Condensate

High pressure steam (150 psig) is generated by two gas boilers and one coal-fired boiler for plant use. Well water is treated by a hot process softener (HPS) and filtered through anthracite filters prior to being fed to the boilers. The high pressure steam is primarily used to lift the hammers at the drop forges, but some may be used for building heat. Before entering the hammer lift cylinders, oil (Citgo Cylinder Oil 680-7) is injected into the steam. The exhaust from the cylinders is captured in the low pressure steam header (6 to 8 psig) and distributed for other uses. The low pressure steam (which has been injected with cylinder oil) is used to heat the HPS (direct steam injection), for anvil heating, and for building heat throughout the facilities. Excess low pressure

steam is exhausted to atmosphere through a baffled separator and multi-port valve to maintain header pressure. The vented flow is measured and has been recorded over recent months. Visual examination of the data indicates that the average venting rate is approximately 12 to 15 million cubic feet per day during drop forge operation.

Condensate from the various area heaters, located throughout the facility, generally flows to the nearest drain and then ultimately to Pond 2. Because of the scattered locations of these heaters, no consideration was given in this study to collecting these streams.

The major sources of oil-contaminated condensate are the baffled separator on the low pressure steam exhaust, the separator on the steam line to the HPS, and the anvil heating lines. These flows have recently been routed to a 1500-gallon horizontal tank from which they drain to Pond 2. Water is drained from near the bottom of the tank through an elevated pipe which can be adjusted to maintain the water level in the tank at approximately 6 to 15 inches.

Mr. Keith Houseknecht, Manager of Plant Engineering for Canton Drop Forge, has estimated the total condensate flow at 3 gpm.

Die lube/condensate

Mineral oil with graphite (DUBRO 500/550) is used on the forge dies and FRESTAPS TO RECIPCE is drained with any condensate collected in the area to a gravity oil/water separator. The separated oil is returned to DUBRO Oil Corporation for reconditioning and returned for reuse. The underflow water is discharged to Pond 2.

No estimate of the flow from this stream is available.

Cooling Water (Recirculating System) Overflow

A recirculating cooling water system is provides cooling water and seal water to the furnaces and cooling water to the hydraulic presses.) After use, the cooling water is collected in a cooling water return sump and returned through a cooling tower to the supply sump. The internals of the cooling tower have been dismantled and removed; now the return stream simply discharges at the top of the tower and free falls to the supply sump. Make-up well water is added to the supply sump based on the level. An overflow pipe from the supply sump discharges to Pond 2.

No estimate of the make-up water requirements is available.

Plant air is provided by an Ingersoll-Rand, water-cooled air compressor. Well water is used in the compressor oil cooler and after-cooler, then discharged to the circulating system supply sump. During the period that Parsons ES

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observed the system operation on 13 May 1997, it appeared that the compressor cooling water supply exceeded the need for make-up water in the recirculating system, as the overflow operated, every time that the return pumps ran. BONTINOUS CY, EVEN WHEN THE D

Coal-fired Boiler Scrubber Discharge

-RECIRCI WATE The coal-fired boiler exhaust is equipped with a scrubber. Four to five gallons per minute (gpm) of well water are sprayed into the top of the tower, 4 while the bulk of the scrubber water is recirculated and treated with lime and polymer. Sludge from the recirculated water tank is pumped to a hopper and excess water overflows to Pond 2. Overflow from the recirculation tank, as well as condensate from the boiler exhaust fan, also flows to Pond 2. The coal-fired boiler (and thus the scrubber system) is not regularly used, but is used periodically every winter. Facility records for January through April 1997 indicate that the coal-fired boiler was used for six days in January and 14 days in March.

Allowing for evaporation, the discharge should be less than the 4 to 5 gallons per minute of well water sprayed into the top of the scrubber.

HPS Blowdown

Chemical precipitates formed in the HPS are discharged to the sanitary sewer system . A 3/4" line runs continuously to limit solids build-up and a larger by line (two or three inch) is manually opened one or two times a shift for a short period to remove larger solids that accumulate in the bottom of the tank. It is reported that lime solids from the process have collected in the sanitary sewer system for distances as great as one mile from the discharge point.

No estimate of the flow rate is available.

Boiler Blowdown

Continuous surface blowdown from the boilers and periodic blowdown of the mud drums is also discharged to the sanitary sewers.

No estimate of the flow rate is available.

Potential Use/Disposal of Process Water and Wastewater Streams

HPS Make-up Water

All boiler feed water is treated in the HPS. Most of the water is sourced from the on-site production wells; the only exception is the amount which results from the condensation of the low pressure steam that is injected into the unit for heating. A simple heat balance (neglecting heat losses through the tank walls and blowdown) indicates that approximately 173,500 gallons of well water and 253,500 pounds of low pressure steam are required per day to generate 1.7

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million pounds of high pressure steam per day (the average production during system operation in April 1997). The condensed steam contributes 30,500 gallons to the boiler feed water stream.

Cooling Water

Once-through cooling water is used in the plant air compressor and then discharged to the recirculating cooling system. Make-up water can also be added to the recirculating system as required. No measurement of either water flow is available. According to the air compressor manufacturer, total heat rejection from the unit is 607,000 BTU/hr. Recommended cooling water flow rates are based on a maximum exit temperature of 120° F. At an inlet water temperature of 60° F (assumed well water temperature), the recommended flow rate would be 20 gpm. Although the flow rate was not measured, it appears that a higher flow rate is used for air compressor cooling. As stated above, it appears that the compressor cooling water discharge exceeds the make-up

Coal-fired Boiler Scrubber Water

requirements of the recirculating system.

The scrubber system uses 4 to 5 gpm of well water when operating.

Since the coal-fired boiler only operates periodically, this water use is not always available.

Water Sampling and Analysis

On 13 May 1997, ten (10) samples were collected from six (6) sampling points (see below) and submitted for chemical analysis and for treatability testing. In addition, pH and temperature measurements were made at several of the sampling points at the same time. The laboratory results reported by Quanterra Environmental Services are attached and are summarized, along with the field data (i.e., pH and temperature), in Table 1. Following is a brief description of each sample point.

O1 Condensate Tank — The sample was collected from a sample valve on the discharge from the 1,500 gallon tank where the three oily condensate streams are combined before discharge to Pond 2.

O2 Pond 3 Influent — The sample was taken from below the surface of the pond in the inlet where the effluent from Pond 2 is discharged into Pond 3.

O3 HPS Separator Discharge — To collect this sample, the discharge from the HPS separator was temporarily routed outside (of the building), through existing piping which previously was used to discharge to Pond 2. The sample represents the discharge from the bottom of the separator and does not include drainage from the steam pipe leading to the separator.

CDFRPT.DOC Page 4 6/6/97 4:46 PM olus press temperchancon

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<u>O4 Boiler Feed Water</u> — The sample was collected downstream of the anthracite filters, at the same location used by the boiler operators for routine boiler feed water tests.

<u>H1 (A and B) HPS Blowdown</u> — The sample was collected from the large blowdown line (on the bottom of the HPS), which is used by the operator for periodic system blowdown. Two samples were required because of different preservatives required for the analyses to be conducted.

<u>H2 (A and B) Boiler Feed Water</u> — Samples were collected at the same location as O4 above. Two samples were required because of different preservatives required for the analyses to be conducted.

Treatability Testing

Two five-gallon buckets of condensate were also collected from the 1,500-gallon tank (same location as sample O1 above). One bucket was sent to KOCH membrane systems for testing and the other was sent to Parsons ES in Syracuse, New York, for screening of other alternatives.

Membrane Filtration

KOCH Membrane Systems treated a portion of the supplied condensate through a membrane filter. They reported that the sample filtered very well, producing a clear filtrate with an O&G concentration of less than 2 mg/L. Samples of the resulting filtrate and concentrate were sent to you for visual observation. In the treatability testing, KOCH did not run the tests for a period long enough to fully concentrate the retentate. They report that the oil and grease (O&G) can be concentrated to about 25% with their hollow fiber unit and to 50% with their tubular unit. For an inlet O&G concentration of 250 mg/L, this represents a 1,000 or 2,000 fold increase in concentration.

KOCH has submitted proposals for both types (i.e., hollow fiber and tubular) of systems. A binder containing these quotes and other information was prepared for you by KOCH and is enclosed.

Screening Tests

Mr. Douglas Morrison, of Parsons ES' Syracuse Office, conducted a number of qualitative tests to identify other methods to potentially remove the oil from the condensate. These are summarized below:

Gravity Separation

Approximately one-third gallon of the condensate sample was allowed to settle over-right. No oil separation was observed.

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Acid Cracking

Sulfuric acid was added to lower the pH to less than 2.0. No separation was observed in the first three to four hours but, after approximately 15 hours, a separate oil layer was observed.

Caustic

Sodium hydroxide was added to raise the pH above 13.0. The sample was checked after approximately 15 hours, but no oil separation was observed.

High Temperature

The sample was heated to above 90° C while mixing. No oil separation was observed during heating or subsequently cooling to room temperature.

Low Temperature

The temperature was decreased to 4° C. After 24 hours, no oil separation was observed.

Alum Addition

A high dosage of aluminum sulfate (alum) was added. There was no immediate effect but, after about 15 hours, a thin oil layer had formed and oily globules were observed at the bottom of the beaker. The middle layer was very clear.

Sodium Chloride Addition

A high dosage of sodium chloride was added to the sample. There was no immediate effect but, after about 15 hours, a distinct oil layer had formed with clear liquid below.

Filtration

An attempt to filter the sample through a 0.45 micron filter was made but the filter blinded almost immediately. A coarser filter (500 to 1,000 microns), generally used by Canton Drop Forge as a pre-filter, was then used and resulted in a clear filtrate and dark retentate. To verify that the retentate was O&G, the filter was rinsed with hexane. The hexane dissolved all of the visible material on the filter indicating that the retentate was O&G. Hexane was also applied to the filtrate to see if additional oil could be visibly removed. No change in appearance of the filtrate was observed.

Simple Filtration

Because of the apparent success of the filtration screening test, the remainder of the sample sent to Syracuse was delivered to a local laboratory for quantitative filtration testing. Samples were filtered using 500 micron, 25 micron, and 10 micron filters. The filtrate from each test was analyzed for O&G and the solids captured on the filter were measured. The results are presented in Table 2.

Table 2
Filtration Testing Results

		THE PROPERTY OF THE PROPERTY O	<u> </u>
	Filter Size	Filtrate O&G	Solids removed by filter
28	No Filter	20 mg/L	-
WAS	500 micron	24 mg/L	<4 mg/L
Jow JED	25 micron	15 mg/L	5,7 mg/L
10 NOOF	10 micron	11 mg/L	9.4 mg/L
116 216			
54 T	These results in	idicate that low effluent O&G	concentrations can be
•			the analysis without filtration

These results indicate that low effluent O&G concentrations can be achieved through coarse filtration. Unfortunately, the analysis without filtration shows an influent O&G concentration of only 20 mg/L as opposed to the 258. mg/L reported by Quanterra Environmental Services. Although the sample was quite aged by the time that these tests were run, it is not anticipated that such a drastic reduction in the O&G concentration could have occurred. Another possibility is that O&G plated out on the plastic liner in the sample bucket used for transport. Again, it is not anticipated that this could result in such a drastic change in concentration. KOCH has since analyzed their sample for comparison; after three (3) weeks (without any steps taken towards preservation) since collection, the results have indicated that 92.9 mg/L of O&G was still present. Obviously, the results above are not consistent with those provided in the laboratory analyses completed by Quanterra and KOCH. The implication of these findings, as indicated in our recommendations, is that on-site testing with the selected technology should be completed prior to final design and installation.

Previously Conducted Tests

Information included in annual reports on boiler water treatment, submitted to Canton Drop Forge by Diversey Water Technologies, indicate that the O&G concentration in the condensate can be reduced to 4 to 13 mg/L through treatment by ferric chloride and polymers.

Evaluation of Alternatives

Wastewater Streams

The estimated volume and quality of the process water and wastewater streams, as they are currently generated, are summarized in Table 3. Information is presented for the period when the forges are operating (generally four days per week).

Table 3
Process Water and Wastewater Streams

	Process v	<u>Mater and Wastewater Stream</u>	ns
Stream	Estimated Flow	Characteristics	Notes
Condensate	3 gpm	O&G = 250 mg/L Temperature is ~ 84° C.	Should be rather clean except for oil because it is derived from steam.
Die Lube/ Condensate	Unknown	May contain oil carry-over if O/W Separator is over- loaded. Residual oil concentration unknown	Apparently good oil separation occurs in the O/W Separator.
Recirculating System Overflow	Unknown	No significant oil contamination. May contain contaminants picked up from furnace seals.	
Coal-fired Boîler Scrubber Discharge	< 5 gpm	May contain contaminants from stack gas. Water is treated with lime and polymer before discharge.	
HPS Blowdown	Unknown	pH = 10, TDS = 310, and Temperature is ~ 100° C. Contains calcium carbonate. May be oversaturated with calcium, resulting in scaling properties.	Is currently discharged to the sanitary sewer.
Boiler Blowdown	Unknown	High purity water with some boiler treatment chemicals and inerts. Temperature is ~ 100° C.	Is currently discharged to the sanitary sewer.

Water Uses

The estimated usage and water quality requirements for candidate recycled water users are presented in Table 4. Information is presented for the period when the forges are operating (generally four days per week).

Table 4 Water Uses

Use	Estimated Flow	Required Water Quality	Notes
HPS Feed Water	173,500 gallons per day (120 gpm)	Restricted to contaminants which can be removed in HPS. System can remove some O&G.	High water temperature is acceptable
Air Compressor Cooling Water	20+ gpm	Non-scaling Non-corrosive <100° F	Required flow rate increases with increasing water temperature
Recirculating Cooling Water	Unknown	Non-scaling Non-corrosive <100° F	
Coal-fired Boiler Scrubber Water	4 to 5 gpm	Non-scaling	

Alternatives

Although further investigation may be warranted, there are no known problems with the process water and wastewater streams, except the oily condensate and the reported solids deposition in the sanitary sewer from the HPS blowdown. The focus of this study is elimination of the soluble oil in the condensate discharge to Pond 2.

Alternatives for disposal of the oily condensate (with or without further treatment) fall in three general categories—continued discharge to the pond system, discharge to the sanitary sewer system, and reuse somewhere at the facility. Treatment alternatives depend on the final disposition of the water and the required water quality. Treatment methods identified, which are effective to some degree for removing oil from the condensate, include membrane filtration, conventional filtration, ferric chloride/polymer treatment, acid treatment, alum treatment, and sodium chloride treatment.

Final Disposal

Discharge to Pond System

If the wastewater stream is discharged to the pond system, one or more environmental permits may be required. Since there is no off-site discharge from the pond system, typical discharge limits prophably do not apply to Canton Drop Forge. Although the limit for O&G in a wastewater discharged directly to a receiving stream is normally about 10 mg/L, the limit may be more restrictive in this case. Discussions with Ohio EPA, which have not been undertaken, would be required to verify the water quality requirements for this option.

Discharge to Sanitary Sewer

The City of Massillon sewer use ordinance limits the O&G concentration of any discharge to 100 mg/L. Other limitations which might impact discharge of the condensate are that the pH can not be less than 5.0 or higher than 10 and the temperature "at the introduction into the City's wastewater treatment plant" cannot exceed 40 degrees Celsius (104° F)". No other known pollutants of concern are in the condensate, but the City may require further testing before accepting the discharge.

Reuse

The four potential locations identified for water reuse are summarized in Table 4. Of these, the two cooling water streams do not appear to be very practical because of the high temperature of the condensate. The condensate would have to be cooled considerably before use as a cooling water.

Reuse in the coal-fired boiler scrubber appears to be possible with limited pre-treatment of the condensate. Because of the intermittent nature of the scrubber operation, this disposal alternative is not available the majority of the time and, therefore, does not provide a means for continuous disposal of the condensate.

The only viable reuse alternative appears to be use as feed water to the HPS. This would require a high degree of oil removal but the high condensate temperature would be an advantage rather than a detriment to the process. Use of hot condensate as part of the feed water would reduce the steam requirement to heat the incoming feed water. A simplified heat balance indicates that the steam requirement would be reduced by approximately 6,000 lb/day.

The major concern with reuse of the condensate is the impact of any residual oil on the receiving system. Membrane-filtered condensate with an oil concentration less than 2 mg/L would probably not impact the system. The HPS system may adequately handle higher concentrations. One concern is the measured O&G concentration of 5.4 mg/L in the boiler feed water. This is near the detection limit for the test and, therefore, may be suspect. However, it is

CDFRPT.DOC Page 10 6/6/97 4:46 PM desirable that the O&G concentration in the boiler feed water be less than 1.0 mg/L. Further testing should be conducted to confirm that the O&G concentration is really this high.

If O&G is getting into the boiler feed water, the most likely source is the low pressure steam used to heat the HPS. The discharge from the separator (on the steam line) to the HPS had a high O&G concentration (although the flow rate was very low), indicating that oil is being carried with the steam to at least that point. Theoretically, reducing the steam use by using hot condensate with low O&G content, would reduce the oil contamination from the source. However, the estimated reduction in steam use is only about 2.5 percent. Flocculant systems are available to remove O&G from boiler feed water, if needed.

Treatment Options

Membrane Filtration

The treatability testing using a membrane filter indicated that the O&G concentration of the condensate can be reduced to less than 2 mg/L. KOCH has proposed two different units that can do the job; however, both require a significant reduction in the condensate temperature because of temperature limitations of the membranes. The hollow fiber system would cost \$34,000 and would require the temperature to be reduced to 113° F or less. This unit has a smaller foot print than the tubular system but can only concentrate the retentate to about 25 percent O&G.

The tubular system costs \$41,500 and requires a temperature reduction to at least 140° F. This unit is capable of concentrating the retentate to approximately 50 percent O&G.

KOCH indicates that higher temperature membranes can be supplied, but they will result in a lesser quality filtrate and will increase the cost of the unit by a factor of 1.5 to 2. Parsons ES has requested information from other manufacturers regarding high temperature membranes.

Conventional Filtration

Conventional filtration appears to provide good oil removal. Based on the tests described above, the O&G in the treated condensate may not be low enough for reuse in the HPS or discharge to the pond system, but would easily meet the City's requirements for discharge to the sanitary sewer. This option can be further evaluated by installing a temporary pump and cartridge filter. The system could be run for a few days to determine the life of the filter cartridges and to obtain additional discharge samples to determine the achievable O&G concentration. A permanent system using a high temperature condensate pump and cartridge filters could be installed for less than \$5,000.

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Chemical Treatment

Testing of a number of chemical treatment options has identified which can reduce the O&G concentration to a low level. Canton Drop Forge has indicated that a primary objective of this effort is to implement a system requiring minimal operator attention. Since these alternatives do not fulfill this requirement, they were not evaluated further.

Alternative Oil for Cylinder Lubrication

Canton Drop Forge is investigating alternative oils for injection into the steam supply to the cylinders, which may be less likely to solubilize in the condensate. This appears to be a worthwhile effort, which may result in an oil that is more readily separated from the condensate and/or may result in less carry-over of oil to the HPS.

Recommendations

The best alternatives for disposal of the condensate appear to be treatment through cartridge filters and discharge to the sanitary sewer or treatment through cartridge filters (or membrane filters, if necessary), and reuse in the HPS. Before pursuing either course of action, the following actions are recommended.

- 1. Monitor the condensate stream to determine the average and peak flow rates. The simplest method of flow measurement would be to operate the 1,500 gallon condensate tank in a fill-and-draw method, while monitoring the time required to fill the tank.
- 2. Install a temporary cartridge filtration system (acquired by borrowing or leasing a unit from a prospective supplier) to evaluate the cartridge change frequency and the sustained effluent quality obtainable.
- 3. If results are satisfactory and it is desired to discharge to the sanitary sewer, discuss proposed discharge with the City of Massillon to define requirements for further testing/applications.
- 4. If it is desired to use treated condensate in the HPS, further sampling of the boiler feed water should be conducted to determine the present O&G concentration. Discussions should be held with the HPS manufacturer, the boiler manufacturer, and/or the boiler water treatment specialists to confirm the limitations on the O&G concentration in the HPS feed water.
- 5. If sufficient O&G reduction cannot be obtained by using a cartridge filter, arrange for on-site testing of one or membrane filters to verify the achievable performance and sizing parameters.

HPS Blowdown

It has been reported that the City of Massillon's sanitary sewer authority is reluctant to accept the condensate flow because of the reported problems with solids deposition from the HPS blowdown. Discharge of lime sludge to sanitary sewer systems is not unusual. The sample analysis of this study indicates that the blowdown is over-saturated with calcium but, because of the calcium carbonate solids in the blowdown, any precipitation probably occurs on the solids rather than on the pipe walls. If solids are building up in the sewer, it probably indicates that there is not sufficient flow to maintain the solids in suspension. Several options are available for improving this situation. These are:

- 1. The point of discharge of the blowdown to the sanitary sewer could be relocated to a place where more flow is present on a continuous basis.
- 2. The blowdown could be modified by eliminating the small continuous blowdown and using only the periodic manual blowdown. Ideally a schedule could be established that would maintain the treated water quality while using less frequent blowdown at a higher flow rate to keep the solids flowing in the sewer. The blowdown could be automated to eliminate dependence on manual operation.
- 3. If it is decided to discharge treated condensate to the sanitary sewer, the additional flow may be used to advantage to assist in keeping the solids flowing in the line.

Summary

In summary, Parsons ES recommends that Canton Drop Forge consider use of cartridge filters for treatment of the oil-contaminated condensate stream. Prior to purchasing and installing a cartridge filtration system, it is recommended that certain measurements and observations be made and a trial application be made. If successful in reducing oil content to the desired levels, the resulting stream can then be discharged to the HPS or the sanitary sewer. This option can be accomplished for \$5,000, or less, provided that the prospective equipment vendor(s) is(are) willing to loan Canton Drop Forge a system for prepurchase treatability testing.

With respect to the HPS blowdown, the recommendations listed above could be implemented. By combining the two streams and, hence, increasing the flow, the HPS blowdown issue may also be resolved.

CDFRPT_DOC Page 13 6/6/97 4:48 PM REMIT PAYMENT TO: File 91849 Los Angeles, CA 90074-1849 Atin: Accounts Receivables

Street Address: 19101 VILLAVIEW ROAD, SUITE 301 CLEVELAND, OHIO 44119

Tel: (216) 486-9005 Fax: (216) 486-6119

INVOICE

2(6)

NOVEMBER 12, 1997

CLIENT REF. :

INVOICE NO. :

00910959

PROJECT NO. :

731549-T1

CLIENT NO.

71275

TO: CANTON DROP FORGE, INC.

4575 SOUTHWAY STREET

CANTON, OHIO

44706

PLEASE REMIT TO:

PARSONS ENGINEERING SCIENCE, INC

FILE 91849

LOS ANGELES, CALIFORNIA

90074-1849

FOR: CANTON DROP FORGE, WASTEWATER RECYCLING

AUTHORIZATION: P.O. #98252 WBS 01000 - INVESTIGATION AMOUNT AUTHORIZED: \$7,000.00

ATTN: MR. KEITH HOUSEKNECHT

BILLING PERIOD: 9/27/97 THROUGH 10/31/97

	CUR. HOURS	CURRENT PERIOD THROUGH 10/31/97	CUM. HOURS	CUMULATIVE-TO-DATE THROUGH 10/31/97
				
WBS 01000 - INVESTIGATION				
DIRECT LABOR	.5	\$4.75	57.1	\$2,022.86
OH & PROFIT @1.95 X D.L.		\$9.26		\$3,944.58
ODCS WITHOUT HANDLING		\$3.81		\$222.56
ODCS W/HANDLING Rate		\$.00		\$496.00
Markup: 5%		\$.00		\$24.80
SUBTOTAL:		\$17.82		\$6,710.80
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TOTAL THIS INVOICE:		\$17.82	y	\$6,710.80
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1

CLIENT REF :

INVOICE NO.: 00910959

PROJECT NO.: 731549-T1

CLIENT NO..: 71275

FORMAT NAME: SBLRLBR15C

	EMPLOYEE NAME	ADJ. DATE	REGULAR HOURS	O/T HOURS	TOTAL HOURS	BILLING RATE	LABOR BILLING	PREMIUM BILLING
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	CLASSIFICATION TOTAL	S	.50		.50		14.01	
	TOTAL LABOR BILLING		50		.50		14.01	

PAGE:

1

CLIENT REF.:

INVOICE NO.: 00910959

PROJECT NO.: 731549-T1

CLIENT NO..: 71275

FORMAT NAME: SBLRLBR11C

W/E DATE EMPLOYEE NAME	EMPLOYEE CLASSIFICATION	ADJ. DATE RATE	REGULAR HOURS	O/T HOURS	TOTAL HOURS
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TOTAL LABOR HOURS			.50		.50

PAGE:

1

DETAIL OF OTHER DIRECT COSTS FOR THE PERIOD ENDING 10/31/97 BY WBS/COST CODE INVOICE NO.: 00910959 PROJECT NO.: 731549-T1

CLIENT NO..: 71275

FORMAT NAME: SBLRFODC03

REF:

REFERENCE NUMBER	DESCRIPTION OF EXPENSES	AMOUNT				
01000: INVESTIGATION						
9540 9550	FREIGHT/EXPRESS/POSTAGE REPRODUCTION CHARGES	2.71 1.10				
	INVESTIGATION					
•	GRAND TOTAL OTHER DIRECT COSTS	3.81				

DETAIL OF OTHER DIRECT COSTS

ER DIRECT COSTS

PAGE:

1

FOR THE PERIOD ENDING 10/31/97 BY JOB/WBS/COST CODE

CLIENT REF.:

INVOICE NO.: 00910959
PROJECT NO.: 731549-T1
CLIENT NO..: 71275
FORMAT NAME: SBLRODCWTT

EQUIP/

	EQUIP							
REF	VEND		INVOICE	DATE			BATCH	
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	00052			10/24/97	POSTAGE		108	.78
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	9551 COPIER CHARGE	ES						
	30270			10/17/97	COPIER	CHARGES	96	1.10
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					INVESTI	OITAE		3.81
					JOB 731	549 TOTAL		3.81
				TOTAL,	OTHER DI	RECT COSTS		3.81

Report Issued To:

Canton Drop Forge PO Box 6902

Canton, Ohio 44706

GEO Job#

9710092(A)

Project Number:

Matrix Type:

Water

Samples Received:

10/17/97

Project Name: Extended Condensate Sampling

Date Analyzed: Analysis Reported:

10/23/97 10/23/97

OIL AND GREASE, TOTAL, RECOVERABLE

Lab#	Date	Station Location	Result	Reporting Limit
5947	10/13/97	12. Condensate tank test point	50.2	5.0
5948	10/14/94	13, Condensate tank test point	156	5.0
5949	10/15/97	14. Condensate tank test point	199	5.0
5950	10/16/97	15, Condensate tank test point	193	5.0
5951	10/16/97	16, Condensate tank test point	176	5.0
5952	10/17/97	17, Condensate tank test point	140	5.0
•			mg/L	ma/L

Analytical Methodology Information

EPA Method 413.1, "Methods for Chemical Analysis of Water and Wastes"

Initial Calibration Date: 10/23/97

Continuing Calibration Date: 10/23/97

Analyst: J. Woodall

ANALYSIS REVIEWED AND APPROVED BY

9263 Ravenna Rd. - Suite A-7 - Twinsburg, Ohio 44087 + Phone 330 963 6990 • Fax 330 963 6975,

10/20/97

CANTON DROP FÖRGE PLANT ENGINEERING WORK ORDER PRINT REPORT

2(4)

Page 1

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4002 745324

5 September 1997

Canton Drop Forge Extended Condensate Sampling

26 16

Purpose:

Collect ten condensate samples over a two week period and analyze for

oil & grease to evaluate the variability of the concentration over time.

Set-up:

Adjust condensate tank discharge line to maintain maximum level of

water in the tank.

Sample collection:

Use 1-liter glass bottles supplied by lab. Collect sample directly in sample bottle--do not transfer from another container. Drain approximately one quart of water through sample line to flush line before collecting sample. Fill bottle approximately to shoulder of bottle. Add acid preservative (supplied by lab) and screw lid on tight. Cool to approximately 4°C (pack in ice) and maintain at that temperature until sample is picked up by laboratory. Work out pick-up schedule with lab to minimize amount of ice you need without requiring excessive trips by lab. Should pick up at least once per week. Twice per week would be good.

Analysis:

Contract with laboratory to analyze samples for Oil & Grease using the partition gravimetric method (EPA Method 413.1). Samples must be analyzed within 28 days of collection (allowable holding time).

How and Test

Laboratories: Quanterra, Inc., North Canton, Rebecca Ştrait (330) 497-9398

This is the lab used in previous studies. Cost was \$45/analysis.

Geo-Analytical, Twinsburg, Amy (216) 983-6990. This lab has quoted \$28 per analysis.

Sampling

Schedule:

Samples should be collected at different times of day to reveal variability that may occur in the oil & grease concentration. One sample should be collected early on Monday when system has been down all week-end and another should be collected late on Friday after system has operated all week. Following is a suggested schedule.

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2-4 p.m. 4-6 p.m.		1	3		1

Note: 1 = week first week; 2 = second week



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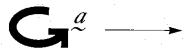
2(6)

SAMPLE	TEMP	DATE	TIME	FLOW	PIPE	-
	128	9/22	2:35	None	12	
2	120	9/29	2:10	Yes	12	PIPE MOD 9/26 FLOW STARTED 9/28
3	155	9/30	4130	LARGE	12	FLOW OUT MUCH GREATER THIN FLOWING. SYSTEM UPON DUE TO SHIFT CHANGE
4	114	10/1	12:57	NORMAL	12	
5	104	10/2	4:43	SMALL	12	
· · · · · · · · · · · · · · · · · · ·	85	10/3	1:30	NONE	12	Boiler OFF
7	120	10/6	7140	Norman	12	The control of the co
8	110	10/7	10:00	Nozma	12	
9	135	10/8	16:29	IGAL IMINIZSEL	12	PUMPED FLOW NOT COUNTED SIFFENSTOPPED
10	145	10/9	8157	and with the second of the control o	12	
//	100	10/10	7:45	NONE	12	Boica OFF
12	82	10/13	10:30	16AL/ 25 sec	12	LOW FLOW FROM MAIN OPENED VALVE MORE
13	123	10/14	3:55	1m. ~535ec	12	
14	121	10/15	4:25	255EC	12	gangawa ay
15	129	10/16	7:30	30 SEC	12	
16	132	10/16	1:37	265EC	12	and the second s
17	97	10/17	11:36	0 5 E C	12	No Flow
	· · · · · · · · · · · · · · · · · · ·	والمواقعة والمعارض وا		ang memengang nganduk mengang nganduk ng mengang nganduk ng mengang nganduk ng mengang ng mengang ng mengang n		



CHAIN OF CUSTODY RECORD

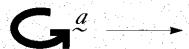
NAME	COMPANY CHUTON TOPOP FORGE NAME AND HO LOA P 6700 ADDRESS 4575 SOUTH WAY 575W CANTON CHIC 44706										OJEC MBER SCRIP		:E	(1Z n	إعلان	s Co	NDE	ENSATE	Garage C	26
SAMPL SIGNA	ER TURES: 🏒		ا الرائز الرائز	<i>'</i>					NO.	73	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \		A	nalys	is Red	queste	ed /	77		·
STA.#	DATE	TIME	COMP	GRAB.	6-7-	STATION L			NO. OF CON- TAINERS		b)/	\angle	\angle	/	\angle		\angle	Temp	NOTES	GAL
	12 10/13/97 10:30 X COMPENSAJETANCTEST POIL										` `					<u> </u>	-	82°F	25	SEC.
	10/19/57			Х	* i			1,	j	Y				ļ				123°F	Imis	Sisec
	olista			X			, å, ,	* f	/_	X				<u> </u>				121°F		255EC
15	10/16/97	7:30		X	9.4	ı.		* _E	/	X								129°F		305EC
16	10/16/97	1:37		X	l i	ř (F &	1	X	- 1			<u> </u>				132°F		165EC
17	10/11/97	11:36		×	H	·	**		/	X						•		97°F	<u> </u>	0566
							<u> </u>	<u> </u>		<u> </u>				*	* .					
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CHAIN OF CUSTODY SIGNATURES (Name, Company, Date, Time) 1. Relinquished By: Received By: 3. Relinquished By:									R	eceive	d By:						·			
	•																			
Rece	Received By:								Re	eceive	d for	Labo	ratory	By:						



CHAIN OF CUSTODY RECORD

COMPANY NAME AND ADDRESS SAMPLER SIGNATURES: SULL SIGNATURES: SULL SIGNATURES: SULL SULL										NU DE	PROJECT NUMBER AND DESCRIPTION: EXTENDED CONDENSINE SAMPE Analysis Requested						PEING		
SIGNA	الله :TURES	ulk	And the second		lower	reck			NO.		10. \ \\ \frac{1}{\supersection \$\chi_{\supersection \text{\$\chi_{\supersection \chi_{\supersection \chi_{\sin \chi_{\supersection \chi_{\supersection \chi_{\supersection \chi_{\supersection \chi_{\supersection \chi_{\supersection \chi_{\supersection \chi_{\sin	7	/ ^	manysi /	S Neu	uesie	3 u	/ 	
STA.#	DATE	TIME	. ₹		STA	TION LOC			NO. OF CONTAINERS OF CONTAINER										ES
1 9/23/97 235PM X CONDENSATE TANK TEST PE										X				ĺ -				128°F	
2	9/29/97	2'10PM	<u> </u>	X	_	*		.,	/	χ								120°F	
3	9/30/77	4:30PM	<u> </u>	X			· ,		/	λ		l				-		/55°F	
4 10/1/97 12:57Pm X " 1 X 1/4°F																			
5 10/2/97 4.45 m × 1 1 X 104° F													,						
6	10/3/97	1,30 Pm		Х	¥ .	· · ·	4 . 	• .	1	X								85°F	
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CHAIN (OF CUSTO	DY SIG	NAT	URE	S (Name, Comp	anv. Date	. Time)	2.98	PA	7		-							
1. Relind	uished By	: K		7Z)	House	VN CEN	COF	-, 10/3	<i>f</i>		alinavi	ichad	Bu-						
Recei	Received By: KE17H Housewern CDF, 10/3/5 2. Relinquished By:																		
3. Relind	uished Bv		_			<u></u>	· · · · · · ·												
						:													
	Received By: Received for Laboratory By:																		

CDF002466



CHAIN OF CUSTODY RECORD

COMPA NAME ADDRE	AND PO	7.5	50	7 6 V 77	OP FORCE 902 HWAY ST S.W. 0410 44706		PROJECT NUMBER AND EXTENDED CONDENSATE SAME DESCRIPTION: EXTENDED CONDENSATE SAME								LING				
SAMPL SIGNA				1:		NO.		5 /	/ /	Aı	nalysi	s Rec	uest	ed /	7				
STA.#	DATE	TIME	COMP	GRAB.	STATION LOCATION	NO. OF CON- TAINERS	0,00									N	OTES		
-7	10/6/97	7:40		X	CONDENSATE TANK TEST POINT	1	X					- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1				12	005	<u>.</u>]
8	10/7/97	10 00		Χ		1	X		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		1.5						OF		
9	10/8/97	10.29		X	4, 4,	1	X										5 PE	min	Jas
10	10/9/97	857	2.0	Х	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1		X									145	S P	<u> </u>	
11	10/10/17	7.45		X	4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	1	X									100	F	<u> </u>	
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				7															8
1. Relin	quished By	ES (Name, Company, Date, Time) CDF, 10/10/97/19237	e.		elinqu eceive										<u> </u>				
and the second s	quished By						4. S	ubmitt	ed to	Labo	ratory	Ву:	·		· .		<u> </u>		
Rece	Received By:						Received for Laboratory By:					<u> </u>							



Report Issued To:

Canton Drop Forge

PO Box 6902

Canton, Ohio 44706

GEO Job#

9710092(A)

Project Number:

Matrix Type:

Water

Samples Received:

10/17/97

10/23/97

Analysis Reported:

Date Analyzed:

10/23/97

Project Name: Extended Condensate Sampling

OIL AND GREASE, TOTAL, RECOVERABLE

Lāb#	Date	Station Location	Result	Reporting
$\frac{1}{\sqrt{2}} \frac{1}{\sqrt{2}} \frac{2}{\sqrt{2}} \frac{2}{\sqrt{2}$			1 1 2	Limit
5947	10/13/97	12, Condensate tank test point	50.2	5.0
5948	10/14/94	13, Condensate tank test point	156	5.0 \
5949	10/15/97	14. Condensate tank test point	∵199 🗎	5.0
5950	10/16/97	15. Condensate tank test point	193	5.0
5951	10/16/97	16. Condensate tank test point	176	5.0
5952	10/17/97	17, Condensate tank test point	140	5.0
				THE WAY
	<u> </u>	医脓腺 医二进剂 医医二二	mg/L	mg/L

Analytical Methodology Information

EPA Method 413.1, "Methods for Chemical Analysis of Water and Wastes"

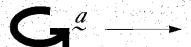
Initial Calibration Date: 10/23/97 Continuing Calibration Date: 10/23/97

Analyst: J. Woodall

CDF002467

ANALYSIS REVIEWED AND APPROVED BY

9263 Ravenna Rd. 🕩 Suite A-7 • Twinsburg, Ohio 44087 • Phone 330



CHAIN OF CUSTODY RECORD 97/0092

	7				77 - 77% F2 / /	. T								-	. , , ,	
COMPA NAME ADDRE	AND PO	0 BOX	50	6	>POP FORGE 902 THWAY 57 5W, 10 44706		Likitet	PROJECT NUMBER AND DESCRIPTION: EXTENDED COND.					NDE	NSATE S	Amplina	
SAMPL SIGNA		//	1/20	/ <u></u>	Rendo	NO. OF					<u> </u>					
STA.#	DATE	TIME	COMP.	GRAB.	STATION LOCATION	CON- TAINERS	G	5)/ _{(*}							TEMP	NOTES/GAL
	10/13/97		ļ <u></u>	X	CONDENSAIETANCTEST POINT		X	53	97						82°F	255EC
13	10/19/57			X.	The State of the S	1	X	55	45	<u></u>				:	123°F	1 min 535EC
14	10/15/17	425		X	April 1980 Brown Company	1	X	58	49			,			121°F	255EC
15	10/16/97	7:30		X	Activities the second	1	X		50						129°F	305EC
16	10/16/97			X	The second secon	1	X	59	51						132°F	265EC
17.	10/17/97	11.36		×		1	X	59	57						97°F	OSEC
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		2010	.		ES (Nama Campany Flata Tima)		. –									

C	HAIN OF CUSTODY SIGNATURES (Name, Company, Date, Time)	
1.	Relinquished By: Cor 10/17/57 1:209 m	2. Relinquished By:
	Received By: Ly 10-17-97 1:10,00	Received By:
3.	Relinquished By:	4. Submitted to Laboratory By: Lis Soul Long 10-17-52 2:30
	Received By:	Received for Laboratory By Allanglis Geo 6/17/91@ 7:20



Report Issued To:

Canton Drop Forge

PO Box 6902

Canton, Ohio 44706 (330)477-2046 (FAX

GEO Job#

9710018(A)

Project Number:

Matrix Type:

Water

Samples Received: 10/03/97

Project Name: Extended Condensate Sampling

Date Analyzed: 10/07/97 Analysis Reported: 10/07/97

OIL AND GREASE, TOTAL, RECOVERABLE

La	b #	Date	· · · · · · · · · · · · · · · · · · ·	Station	Location	\	Result	Reporting
Š								Limit
56	71	09/22/97	1,	Condensate	Tank Test F	⊃oint -⊲	134	5.0
56	372	09/29/97	2.	Condensate	Tank Test F	Point	35.2	5.0
56	373	09/30/97	3,	Condensate	e Tank Test i	Point	14.2	5.0
56	374	10/01/97	4.	Condensate	Tank Test	Point 🕖 👉	23.9	5.0
56	375	10/02/97		Condensate	The state of the s	1 1 1	57.0	5.0
56	376	10/03/97		Condensate			111	5.0
					24 -		= 100	Letter Comment
		- **	4	1. 在某点点			mg/L	mg/L

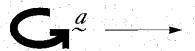
Analytical Methodology Information

EPA Method 413.1, "Methods for Chemical Analysis of Water and Wastes"

Initial Calibration Date: 10/07/97 Continuing Calibration Date: 10/07/97

Analyst: J. Woodall

ANALYSIS REVIEWED AND APPROVED BY



CHAIN OF CUSTODY RECORD 9710018

NAME ADDRE	COMPANY NAME AND PO BOX 5 6902 ADDRESS 4875 500TH WAY 57 5W SAMPLER SIGNATURES: Beilly Louiseness						NUI DES	PROJECT NUMBER AND DESCRIPTION: EXTENDED CONDENSITE SAMPL Analysis Requested						DENSATE SAMPLING	
STA.#	DATE	TIME	COMP	GRAB.	STATION LOCATION	CON- TAINERS	010								NOTES
1	9/22/97	2:35 PM		X	CONDENSATE TANK TEST POINT	- 1	X		56	71					128°F
	9/29/97			X.		1 -	χ		56	72					120°F
Э	9/30/97	4:30 PM	\	X	the second second second	1	X		_	<i>13</i>		:			155°F
4	10/1/97	12:57Pm	1	X	A Company of the Comp	1	X		56	74				· .	114°F
5_	10/2/97	4:43 PM		×	The state of the s	/	X		56	<i>15</i>					104°F
6	10/3/97	1:30 PM		X		1	X		56	76					85°F
	_					47.5									
			<i>a</i>	, 1					100		. :	1.0.			
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CHAIN	OF CUSTODY S	IGNATUR	ES (Name, C	ompany, Date,	Time) 2/	18 PM	•				
I. Relir	nquished By:/	5E777	1 HOU	SCHOUR	-CVI-, 10	13/51 2	Relinquished By:				
Rece	eived By: <u> </u>	day b	Cas 10-	3.97 2:4	18		Received By:	· · ·			
3. Relir	nquished By:	· · · · · · · · · · · · · · · · · · ·			<u> </u>	4.	Submitted to Labo	ratory By:	The fice	Jul 10-3	-97 4:70
Rece	eived By:		·	- · · · · · · · · · · · · · · · · · · ·			Received for Labo	ratory By:(Ullinge	les 650 10	V397@ 42
						•			\sim \sim O		



Report Issued To:Canton Drop Forge PO Box 6902 Canton, Ohio 44706 (330) 477-2046 (FAX)

2(b)

Extended Condensate Sampling

GEO Job# 97

9710062(A)

Project Number:

Project Name:

Matrix Type:

Water

Samples Received:

10/10/97

Date Analyzed:

10/14-15/97

Analysis Reported:

10/15/97

OIL AND GREASE, TOTAL, RECOVERABLE

Lab#	Date		Station Location	Result	Reporting
			The John Style Style		Limit
5842	10/06/97	7,	Condensate Tank Test Point	114	5.0
5843	10/07/97	8,	Condensate Tank Test Point	-33.1	5.0
5844	10/08/97	9,	Condensate Tank Test Point	185	5.0
5845	10/09/97	10	Condensate Tank Test Point	317	5.0
⊆5846 [∑]	10/10/97	' 11	Condensate Tank Test Point	213	5.0
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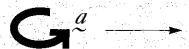
Analytical Methodology Information

EPA Method 413.1, "Methods for Chemical Analysis of Water and Wastes"

Initial Calibration Date: 10/14-15/97 Continuing Calibration Date: 10/14-15/97

Analyst: J. Woodall

ANALYSIS REVIEWED AND APPROVED BY



CHAIN OF CUSTODY RECORD 9710062

NAME ADDRI	MPANY CANTON DROP FORCE ME AND POBOX = 6902 DRESS 4575 SOUTH WAY ST S.W. CANTON, OHIO 44706 MPLER MATURES:						PRI NU DE:	OJEC MBER SCRIF	T R AND PTION	<u> </u>	<u> </u>		1973		DENS	ATE SAMPLING	- Mari	
				1 - 1 - 1 - 1 - 1 - 1 - 1		NO. OF	\ <u>\</u> _{\delta}	o's m'		Ana		Analysis Requested			ed /	7		-
STA.#	DATE	TIME	COMP	GRAB.	STATION LOCATION	CON- TAINERS	S P	m/								NOTES		
7	10/6/97	7:40		X	CONDENSATE TANK TEST POINT	ì	X		58	42		1	12			120°F		
8	10/7/97	10 00		X	The state of the s	1	X		58	43	- 10 - 1					1100E		
9	10/8/97	10,29		X	Entre to the second		X		58	44						135 °F min	Jas	
10	10/9/97	8.50		X	On the second of the second	- 1	X	:	58	45						145 °F		
//	10/10/97	7:45		X		1	X		58	26					e e e e e e e	100 °F		
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MAIN	() -	111511117	SIGNATUR	⊢ S∵/Niama	t :nmnani	/ IIIato	IIMA
	\sim	0001001	OIGITALIOLI		CUITIDATI	r. Dail.	1111101

1. Relinquished By	1SEKNETH	T CDE	<u>e, ioliot</u>	97/2/	2372
Received By:	Week.	60010	2/10/97 C	0/2:2	3 <i>P</i> m
3. Relinquished By:		· · · · · · · · · · · · · · · · · · ·		<u> </u>	-
Received By:		*			

2. Relinquished By: _	 	•	
· · · · · · · · · · · · · · · · · · ·		 	
Received By:	1.0	100	

4.	Submitted to Laboratory By:	Ulan	aftin Geo	010/10P7	@1:53PM
	Received for Laboratory By:	Mul	mast	1010.97	1.50PM.

Ģ

Report Issued To:

Canton Drop Forge

PQ Box 6902

Canton, Ohio 44706 (330)477-2046 (FAX

GEO Job#

9710018(A)

Project Number.

Matrix Type:

Water

Samples Received: Date Analyzed:

10/03/97 10/07/97

10/07/97

Analysis Reported:

Project Name: Extended Condensate Sampling

OIL AND GREASE, TOTAL, RECOVERABLE

Lab#	Date	Station Location	Result	Reporting Limit
5671	09/22/97	1. Condensate Tank Test Point	134	5.0
5672	09/29/97	2, Condensate Tank Test Point	35.2	5.0
5673	09/30/97	3, Condensate Tank Test Point	14.2	. 5.0
5674	10/01/97	4. Condensate Tank Test Point	23.9	5.0
5675	10/02/97	5, Condensate Tank Test Point	57.0	5.0
5676	10/03/97	6, Condensate Tank Test Point	111	5.0
-	,	le le	mg/L	ma/L

Analytical Methodology Information

EPA Method 413.1, "Methods for Chemical Analysis of Water and Wastes"

Initial Calibration Date: 10/07/97 Continuing Calibration Date: 10/07/97

Analyst: J. Woodall

ANALYSIS REVIEWED AND APPROVED BY

G^a

Report Issued To:Canton Drop Forge PO Box 6902 Canton, Ohio 44706 (330) 477-2046 (FAX) 26

GEO Job#

9710062(A)

Project Number:

Matrix Type: Samples Received:

Water 10/10/97

Project Name:

Extended Condensate Sampling

Date Analyzed:

10/14-15/97

Analysis Reported:

10/15/97

OIL AND GREASE, TOTAL, RECOVERABLE

Lab#	, Date	Station Location	Result	Reporting Limit
5842	10/08/97	7. Condensate Tank Test Point	114	5.0
5843	10/07/97	8, Condensate Tank Test Point	33.1	5.0
5844		9. Condensate Tank Test Point	185	5.0
5845		10, Condensate Tank Test Point	317	5.0 \ BERD
5846	10/10/97	11, Condensate Tank Test Point	213	5.0
			,mg/L	mg/L

Analytical Methodology Information

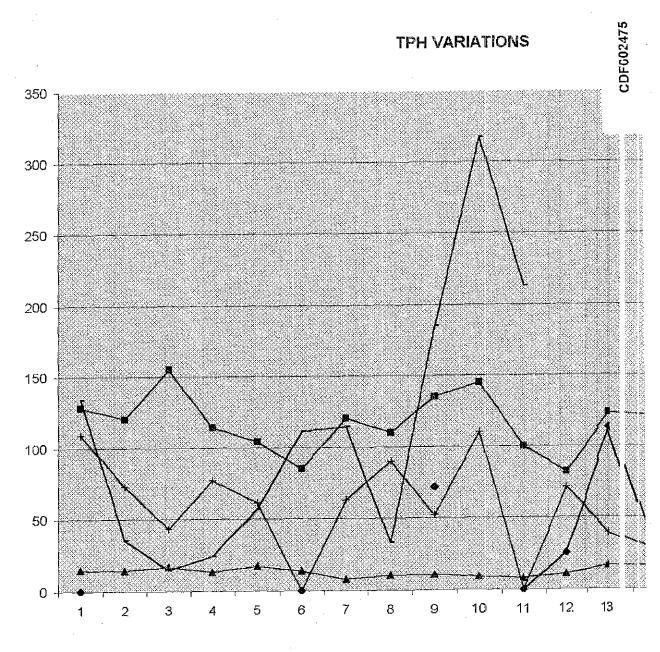
EPA Method 413.1, "Methods for Chemical Analysis of Water and Wastes"

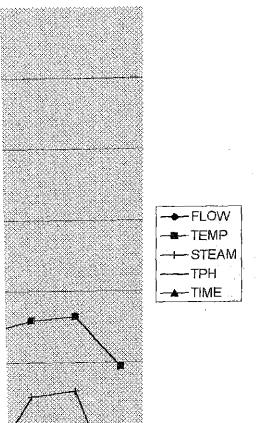
Initial Calibration Date: 10/14-15/97 Continuing Calibration Date: 10/14-15/97

Analyst: J. Woodall

ANALYSIS REVIEWED AND APPROVED BY

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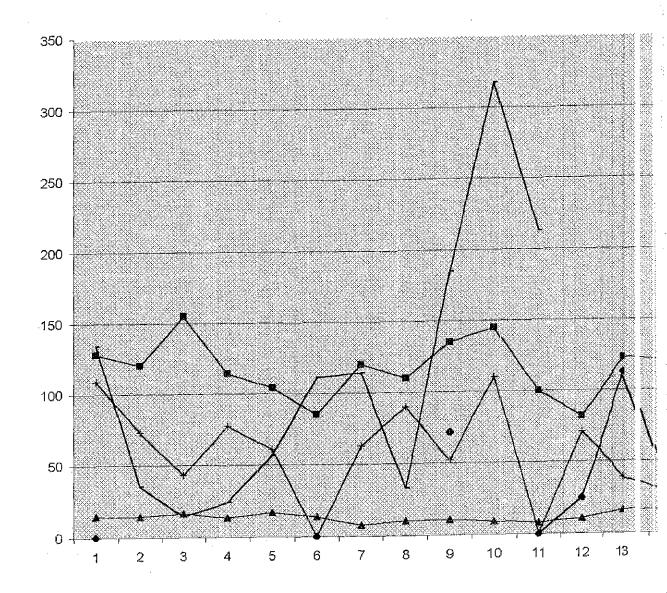




SAMPLE							AMBIENT		
NUMBER	DATE	DAY		TIME	FLOVV	TEMP	TEMP	HUMIDITY	OI.
1	22-Sep	MON	14:35	14.58	Ö	128			
2	29-Sep		14:10	14.17		120			
3	30-Sep		16:30	16.5		155			
4	1-Oct	WED	12:57	12.95		114			
5	2-Oct	THU	16:43	16.72		104			
6	3-Oct	FRI	13:30	13.5	. 0	85			
7	6-Oct	MON	7:40	7.67		120			
8	7-Oct	TUE	10:00	10		110			
9	8-Oct	WED	10:29	10.48	7:2	135			
10	9-Oct	THU	8:57	8.95		145			
11	10-Oct	FRI	7:45	7.75	Ö	100			
12	13-Oct	MON	10:30	10.5	25	82			
13	14-Oct	TUE	15:55	15.92	113	123	•		
14	15-Oct	WED	16:25	16.42	25	121			
15	16-Oct	THU .	7:30	7.5	30	129		• .	
16	16-Oct	THU	13:37	13.62	26	132			
17	17-Oct	FRI	11:36	11.6	0	97			

CDF002476

TPH VARIATIONS



T	OUTPUT	STEAM	TPH
55	54	109	134
36	37	73	35.2
23	20	43	14.2
37	40	77	23.9
29	32	61	57
0	0	0	111
3 0	33	63	114
44	46	90	33.1
25	27	52	185
55	5 5	110	317
0	0	0	213
34	37	<u>, 71</u>	
18	21	39 -	e.
10	17	27	
38	38	76	
38	42	80	
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#2 BOILER#3